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Applied Catalysis A: General 323 (2007) 104-109

www.elsevier.com/locate/apcata

Effect of Co addition for carburizing process of Ti-oxide/SiO₂ into TiC/SiO₂

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> Received 27 December 2006; received in revised form 29 January 2007; accepted 5 February 2007 Available online 16 February 2007

Abstract

Lowering the carburization temperature of Ti-oxide into TiC down to 1173 K could be achieved by the addition of Co. Co-promoted TiC/SiO₂ catalysts were prepared by the temperature programmed reaction (TPR) method. Co–Ti/SiO₂ precursors were prepared by use of the successive impregnation method (sc) and the co-impregnation method (co). Samples were characterized by X-ray absorption fine structure (XAFS) measurements and X-ray diffraction (XRD) results. The carburization degree of TiC was affected by the method of Co addition. The carburization degree of sc Co–TiC/SiO₂ was better than that of co Co–TiC/SiO₂. The activity of thiophene hydrodesulfurization reaction at 693 K on sc Co–TiC/SiO₂ was higher than that on co Co–TiC/SiO₂. The HDS activity was related to the carburization degree of TiC. \bigcirc 2007 Elsevier B.V. All rights reserved.

Keywords: TiC catalyst; XAFS; Co additive; Carburization

1. Introduction

Small atoms, such as carbon or nitrogen, dissolved interstitially in the lattices of early transition metals produce a class of compounds with unique physical and chemical properties [1,2]. These interstitial compounds are referred to as early transition metal carbides (ETMC) and nitrides (ETMN). ETMC and ETMN were found to have similar activities to those of the group 8–10 metals (Pt, Pd, Rh, etc.) [3–6].

Most of works on the catalytic applications of ETMC have been focused on Mo₂C and WC [7–10]. In contrast, very few works have been reported on the groups 4 and 5 metal carbides such as TiC and NbC [11–14]. The focus on Mo₂C and WC has occurred in part because they could be prepared with high surface areas at moderate synthesis temperatures in the range between 900 K and 1100 K [7–10]. On the other hand, it has been reported that the carburization of bulk TiO₂ into TiC requires a high temperature; 1410 K [5]. Using high temperature caused a sintering of TiC, and decreased the surface area of TiC. The lowering of carburizing temperature is required for the catalytic

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application of TiC. We have demonstrated that the carburizing temperature could be lowered by supporting the metal species on amorphous silica [15,16].

Co addition could be expected to promote the carburization with activating methane by dehydrogenation because it has been used for Fischer-Tropsch catalysts [17]. In this work, in order to lower carburization temperature, we added Co to TiO₂, and then demonstrated carburization. In addition, Co-TiC/SiO₂ was prepared. For the preparation of Co-Ti/SiO₂, two different methods were applied. One is successive impregnation method (sc), and the other is co-impregnation method (co). Co-Ti/SiO₂ precursors were carburized by using temperature programmed reaction (TPR) method. Carburization degree of Ti was characterized by using Ti K-edge XAFS (X-ray absorption fine structure) measurements. In order to investigate the effect of Co addition, Co K-edge XAFS was also measured. Thiophene HDS (hydrodesulfurization) reactions were demonstrated to investigate the relationship between the carburization degree of TiC activity and the HDS.

2. Experimental

 $Co-Ti/SiO_2$ precursors were prepared by sc method (sc Co-Ti/SiO₂) and co method (co Co-Ti/SiO₂). The preparation

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process of sc Co–Ti/SiO₂ consisted of two stages. First, intermediate precursors of Ti/SiO₂ were obtained by impregnating SiO₂ (Aerosil, #200) with TiCl₄/HCl solutions at RT for 24 h. To decompose the titanium chloride, we calcined the intermediate precursor at 623 K in air for 2 h. Second, Co–Ti/SiO₂ was obtained by impregnating Ti/SiO₂ with aqueous cobalt chloride solution at RT for 24 h. To decompose the cobalt chloride, we calcined the precursor at 623 K in air for 2 h. Ti loading was regulated to 5 wt% with a Co/Ti molar ratio of 0.25. The co-impregnation catalyst was prepared as follows: an HCl aqueous solution of TiCl₄ and CoCl₂ was impregnated with SiO₂ at RT for 24 h. To decompose the titanium chloride and the cobalt chloride, we calcined the precursor at 623 K in air for 2 h. SiO₂ at RT for 24 h. To decompose the titanium chloride and the cobalt chloride, we calcined the precursor at 623 K in air for 2 h. Co–Ti/SiO₂ at RT for 24 h. To decompose the titanium chloride and the cobalt chloride, we calcined the precursor at 623 K in air for 2 h. Co–Ti/SiO₂ at RT for 24 h. To decompose the titanium chloride and the cobalt chloride, we calcined the precursor at 623 K in air for 2 h. Co–Ti/SiO₂).

The Co–Ti/SiO₂ precursor was carburized in a 20% CH₄/H₂ mixed gas stream to produce Co–TiC/SiO₂ in the TPR process. This process involves two steps: (1) raising the temperature at a linear rate of 10 K min⁻¹ to 1273 K and (2) maintaining the sample at the final temperature for a certain period.

XAFS spectra at Ti K-edge and Co K-edge were measured at RT in transmission mode at BL-10B (Co K-edges), BL-7C, 9C and 12C (Ti K-edges) using the Photon Factory in the Institute of Material Structure Science, High Energy Accelerator Research Organization (PF, IMSS-KEK) (Proposals nos. 2002G116, 2005G214). Synchrotron radiation emitted from a 2.5 GeV storage ring was monochromatized by a Si(3 1 1) channel cut monochromator or a Si(111) double crystal monochromator at BL-10B or BL-7C, 9C, 12C, respectively. Each sample was pressed into a pellet, which was 10 mm in diameter. Curve-fitting analysis of EXAFS oscillations was conducted by the EXAFS analysis program REX2000 (Rigaku Co.). Model parameters for curve-fitting analysis (back scattering amplitude and phase shift functions) were extracted from EXAFS oscillations observed for standard materials (TiO₂, TiC, CoTiO₃, Co foil, Co₃O₄ and CoS), or they were created by FEFF.

The XRD (X-ray diffraction) analysis (Bruker axs, MXP3) was also carried out. HDS of thiophene was performed in continuous flow system interfaced to a gas chromatograph (SHIMADZU, GC-8A) with a TCD detector. The main products were 1-butene and 2-butene. The catalyst (0.4 g) was pretreated under H₂ flow (10 ml min⁻¹) for 0.5 h at 1073 K or 773 K, prior to use. HDS reaction was monitored under 2.8% thiophene/H₂ (5 ml min⁻¹) at 693 K.

3. Results and discussion

3.1. Carburization of bulk TiO_2

XRD patterns of TiO₂, TiC, carburized TiO₂ and carburized Co–TiO₂ are shown in Fig. 1. In the case of carburized TiO₂, the Ti₃O₅ phase was observed and no peak attributed to TiC was appeared. On the other hand, the patterns for carburized Co–TiO₂ showed TiC phase clearly. Such results mean that TiO₂ was not carburized at 1273 K without Co additive, but was carburized to produce TiC with Co additive. In the case of carburized Co–TiO₂, Co metal phase was observed as well as

2000cps • TiC Ti₃O₅ $\triangle Co$ (a) ntensity (b)(c (ď 30 50 70 20 40 60 2θ / degree

Fig. 1. XRD patterns of (a) carburized Co–TiO₂, (b) carburized TiO₂, (c) Co–TiO₂ and (d) bulk TiO₂.

TiC phase. It was found that Co oxide was reduced to Co metal during the carburization. We supposed that the carburization of TiO_2 proceeded focusing around reduced Co.

In order to optimize the carburization condition, we prepared carburized Co-TiO₂ by controlling the carburization temperature and the retention time. Fig. 2 shows XRD patterns of carburized Co-TiO₂ as a function of carburization temperature (1273 K, 1223 K, 1173 K and 1073 K). The XRD pattern of Co-TiO₂ carburized at 1073 K shows only Ti₃O₅ phase. It can be said that TiC was not formed by a carburization temperature as low as 1073 K. In the case of Co-TiO₂ carburized at 1173 K, however, TiC phase was observed slightly besides the main Ti₃O₅ phase. It was found that TiC was formed by the carburization above 1173 K. In other words, the carburization temperature of Ti-oxide into TiC could be lowered down to 1173 K by addition of Co. In the case of Co-TiO₂ carburized at 1223 K, the TiC phase was larger compared to the case of Co-TiO₂ carburized at 1173 K. Raising the carburization temperature up to 1273 K, we could distinctly observed the TiC phase



Fig. 2. XRD patterns of carburized Co–TiO₂ varied with the carburization temperature: (a) 1273 K, (b) 1223 K, (c) 1173 K and (d) 1073 K.



Fig. 3. XRD patterns of carburized $Co-TiO_2$ (carburization temperature = 1173 K) maintained for (a) 120 min, (b) 80 min and (c) 40 min.

and the Ti₃O₅ phase disappeared. The carburization degree from Ti-oxide to TiC became higher as the carburization temperature increased. Fig. 3 shows that XRD patterns of carburized Co–TiO₂ (carburization temperature = 1173 K) varied with the retention time (40 min, 80 min and 120 min). They included Ti₃O₅ phase and very weak TiC phase. Almost no differences are found among the three samples. It was supposed that the retention time has less dependence on the carburization degree compared to the carburization temperature.

3.2. Carburization of TiO₂/SiO₂

In the supported system, the carburization condition was regulated as follows: the carburization temperature is 1273 K and the retention time is 30 min. Co-promoted TiC/SiO₂ catalysts were prepared by the carburization of Co–Ti/SiO₂ precursors.

Ti K-edge XAFS measurements were carried out to determine the electronic state and the local structure of the



Fig. 4. Fourier transforms of k^3 -weighted Ti K-edge EXAFS oscillations for (a) sc Co–TiC/SiO₂, (b) co Co–TiC/SiO₂, (c) TiC and (d) TiO₂.

Table 1 Curve-fitting results for Ti–C and Ti–(C)–Ti coordination on Co–TiC/SiO₂ catalysts

Sample	Coordination	CN	<i>r</i> (nm)	dE_0 (eV)	DW (nm)
sc Co–TiC/SiO ₂	Ti–C	3.6	0.212	-4.07	0.0067
	Ti–(C)–Ti	6.1	0.303	-4.96	0.0070
co Co-TiC/SiO ₂	Ti–C	2.0	0.205	12.60	0.0054
	Ti–O	1.2	0.212	-16.21	0.0073
	Ti–(C)–Ti	3.2	0.301	-8.95	0.0072
Bulk TiC (model)	Ti–C	6	0.217	0	0.0060
	Ti–(C)–Ti	12	0.306	0	0.0060

catalysts. Fig. 4 shows the FT (Fourier transform) of k^3 weighted EXAFS oscillations for Co-TiC/SiO₂ catalysts. CF (curve-fitting) analysis was carried out by using the bulk TiC as the reference compound to determine CN (coordination number) and the coordination distance. FT profiles of both sc Co-TiC/SiO₂ and co Co-TiC/SiO₂ are similar to that of bulk TiC. The CF results are listed in Table 1. CN values of Ti-C and Ti-O were different for sc Co-TiC/SiO₂ and for co Co-TiC/ SiO₂. In the case of sc Co-TiC/SiO₂, CN values of Ti-C and Ti-O were 3.6 and 0.0, respectively. In the case of co Co-TiC/SiO₂, however, CN values of Ti-C and Ti-O were 2.0 and 1.2, respectively. It was found that Ti-oxide was still remained on co Co-TiC/SiO₂. It was supposed that the carburization degree of sc Co-TiC/SiO₂ was better than that of co Co-TiC/SiO₂. CN values of Ti-(C)-Ti for sc Co-TiC/SiO2 and co Co-TiC/SiO2 were 6.1 and 3.2, respectively. CN of Ti-(C)-Ti correlates with the TiC particle size. And hence, the particle size of sc Co-TiC/ SiO₂ seems to be larger than that of co Co-TiC/SiO₂. CN values of Ti-(C)-Ti coordination for both Co-TiC/SiO₂ were less than that for bulk TiC (CN = 12). It was suggested that TiC on Co-TiC/SiO₂ were highly dispersed on the SiO₂ surface. To explain the difference of the carburization degree, we carried out Ti Kedge XAFS measurements for Co-Ti/SiO₂ precursor. Fig. 5 shows the FT of k^3 -weighted EXAFS oscillations for Co–Ti/ SiO₂ precursors. CF analysis was carried out by using the bulk



Fig. 5. Fourier transforms of k^3 -weighted Ti K-edge EXAFS oscillations for (a) sc Co–Ti/SiO₂, (b) co Co–Ti/SiO₂, (c) TiO₂ (anatase) and (d) TiO₂ (rutile).

Table 2 Curve-fitting results for Ti–O and Ti–(O)–Ti coordination on Co–Ti/SiO₂ catalysts

Sample	Coordination	CN	<i>r</i> (nm)	dE_0 (eV)	DW (nm)
sc Co–Ti/SiO ₂	Ti–O	3.7	0.190	-3.12	0.0072
	Ti-(O)-Ti	1.4	0.301	-12.42	0.0073
	Ti-(O)-Ti	1.4	0.345	6.24	0.0068
co Co–Ti/SiO ₂	Ti–O	3.8	0.191	-6.02	0.0064
	Ti-(O)-Ti	2.3	0.296	-16.86	0.0081
	Ti-(C)-Ti	1.6	0.345	3.88	0.0067
Bulk TiO ₂ (model, anatase)	Ti–O	6	0.196	0	0.0060
	Ti-(O)-Ti	4	0.304	0	0.0060
	Ti-(O)-Ti	4	0.379	0	0.0060

Table 3

Curve-fitting results for Co–O, Co–(O)–Co and Co–(O)–Ti coordination on Co–Ti/SiO₂ catalysts

Sample	Coordination	CN	<i>r</i> (nm)	dE_0 (eV)	DW (nm)
sc Co–Ti/SiO ₂	Co–O	4.9	0.197	-2.75	0.0058
	Co-(O)-Co	3.1	0.286	5.76	0.0062
	Со-(О)-Со	2.9	0.336	5.47	0.0054
co Co–Ti/SiO ₂	Co–O	5.1	0.197	-20.41	0.0098
	Co-(O)-Ti	0.86	0.350	-5.79	0.0056
	Co-(O)-Ti	0.97	0.405	-10.46	0.0051
Bulk Co ₃ O ₄ (model)	Co–O	1.3	0.181	0	0.0060
	Co–O	4	0.199	0	0.0060
	Со-(О)-Со	4	0.287	0	0.0060
Bulk CoTiO ₃ (model)	Co–O	6	0.214	0	0.0060
	Co-(O)-Ti	6	0.253	0	0.0060
	Co-(O)-Ti	6	0.273	0	0.0060

TiO₂ as the reference compound [18]. The results are listed in Table 2. Both Co–Ti/SiO₂ precursors showed structures similar to that of rutile TiO₂. It was found that Ti species in Co–Ti/SiO₂ precursor are in the rutile phase TiO₂, and no clear difference was observed between sc Co–Ti/SiO₂ and co Co–Ti/SiO₂ precursors. The carburization degree of TiO₂ was affected not by the phase of precursor TiO₂, but by the state of concomitant Co. Thus, Co K-edge XAFS measurements were carried out for Co–Ti/SiO₂ precursor (Table 3).

Fig. 6 shows Co K-edge XANES spectra of Co–Ti/SiO₂ precursors, Co₃O₄ and CoTiO₃. A strong absorption band around 7730 eV and 7725 eV was observed in XANES spectra for Co₃O₄ and CoTiO₃, respectively. From the XANES profile, the states of Co in sc Co–Ti/SiO₂ and co Co–Ti/SiO₂ were similar to those in Co₃O₄ and CoTiO₃, respectively.

Fig. 7 shows Co K-edge XANES spectra of Co–TiC/SiO₂ and Co foil. The XANES profiles of Co–TiC/SiO₂ catalysts were more similar to that of Co foil than to that of Co oxide. It was supposed that Co oxide was reduced to the metal for Co– TiC/SiO₂ during the carburization process. No difference was observed in XANES profiles between sc Co–TiC/SiO₂ and co Co–TiC/SiO₂. Since the XANES profile of Co–TiC/SiO₂ differed from that of Co foil at around 7745 eV, it was supposed that Co of Co–TiC/SiO₂ was in the Co–Ti alloy or CoC_x species [19].

Fig. 8 shows the FT of k^3 -weighted Co K-edge EXAFS oscillations for Co–Ti/SiO₂ precursor. The FT profile of sc Co–

Ti/SiO₂ resembled that of bulk Co₃O₄. On the other hand, the FT profile of co Co–Ti/SiO₂ was not similar to that of Co₃O₄ but was close to that of CoTiO₃. CF analysis was carried out by using bulk Co₃O₄ and CoTiO₃ as the reference compound [20]. The CN (Co–(O)–Co) of sc Co–Ti/SiO₂ (3.1) was less than that of Co₃O₄ (4.0). It was supposed that Co₃O₄ on sc Co–Ti/SiO₂ was dispersed, and that small Co₃O₄ clusters were formed at the TiO₂ surface. In the case of co Co–Ti/SiO₂, CN (Co–(O)–Ti)



Fig. 6. Co K-edge XANES spectra of (a) sc Co–Ti/SiO₂, (b) co Co–Ti/SiO₂, (c) Co₃O₄ and (d) CoTiO₃.



Fig. 7. Co K-edge XANES spectra of (a) sc Co–TiC/SiO₂, (b) co Co–TiC/SiO₂ and (c) Co foil.



Fig. 8. Fourier transforms of k^3 -weighted Co K-edge EXAFS oscillations for (a) sc Co–Ti/SiO₂, (b) co Co–Ti/SiO₂, (c) Co₃O₄ and (d) CoTiO₃.

was much less than that of $CoTiO_3$. It was supposed that $CoTiO_3$ on co $Co-Ti/SiO_2$ was highly dispersed, formed at the surface and the inside of TiO_2 .

Fig. 9 shows the FT of k^3 -weighted Co K-edge EXAFS oscillations for Co–TiC/SiO₂ catalysts. The FT profiles of both Co–TiC/SiO₂ showed some similarity to that of Co foil. CF analysis was carried out by using the Co foil as the reference compound; the results are listed in Table 4. The main peak at around 0.2 nm was attributed to Co–Co coordination. CN values (Co–Co) of sc Co–TiC/SiO₂ (6.8) and co Co–TiC/SiO₂ (6.9) were smaller than that of Co foil (12). It seems that Co on Co–TiC/SiO₂ was still dispersed after the high temperature carburization treatment. Taking into account the larger DW

Table 4 Curve-fitting results for Co–Co coordination on Co–TiC/SiO₂ catalysts



Fig. 9. Fourier transforms of k^3 -weighted Co K-edge EXAFS oscillations for (a) sc Co–TiC/SiO₂, (b) co Co–TiC/SiO₂ and (c) Co foil.



Scheme 1. Plausible structure of carburization process from sc Co–Ti/SiO $_2$ into sc Co–TiC/SiO $_2$.

factor for Co–TiC/SiO₂ (*ca.* 0.009 nm), it can be said that the Co lattice of Co–TiC/SiO₂ distorted and that the distortion was derived from carbon and Ti dissolved interstitially in the Co lattice. It can be said that TiO_2 would be carburized at around the reduced Co site.

From the above results, plausible structures for Co–Ti/SiO₂ precursor and Co–TiC/SiO₂ catalysts were suggested. Scheme 1 displays the carburization process of sc Co–Ti/SiO₂ into sc Co–TiC/SiO₂. Scheme 2 displays the carburization process of co Co–Ti/SiO₂ into co Co–TiC/SiO₂. In the case of sc Co–Ti/SiO₂, Co₃O₄ was formed at the surface of TiO₂. During the carburization process, Co oxide was reduced and acted as a carburization center for TiO₂ into TiC.

A Co–Ti mixed oxide, such as CoTiO₃, was formed at the surface and on the inside of TiO₂ on the co Co–Ti/SiO₂. Because of the chemical stability of Co–Ti mixed oxide, Co–Ti mixed oxide was hardly reduced during the carburization.

Coordination	CN	<i>r</i> (nm)	dE_0 (eV)	DW (nm)	
Co–Co	6.8	0.251	-16.61	0.0091	
Co–Co	6.9	0.250	-25.46	0.0090	
Co–Co	12	0.251	0	0.0060	
	Coordination Co–Co Co–Co Co–Co	CoordinationCNCo-Co6.8Co-Co6.9Co-Co12	Coordination CN r (nm) Co-Co 6.8 0.251 Co-Co 6.9 0.250 Co-Co 12 0.251	Coordination CN r (nm) dE ₀ (eV) Co-Co 6.8 0.251 -16.61 Co-Co 6.9 0.250 -25.46 Co-Co 12 0.251 0	



Scheme 2. Plausible structure of carburization process from co Co-Ti/SiO₂ into co Co-TiC/SiO₂.



Fig. 10. HDS profiles on Co-TiC/SiO₂ catalysts.

Considering that the carburization of TiO₂ proceeds around reduced Co species, added Co did not effectively work to carburize Ti-oxide on co Co–TiC/SiO₂. So the TiC and Co with a little amount of carbon and Ti dissolved were formed in the lattice and a slight amount of Ti-oxide remained on the co Co– TiC/SiO₂. Since Ti-oxide remained on co Co–TiC/SiO₂, one can conclude that the carburization degree of sc Co–TiC/SiO₂ was better than that of co Co–TiC/SiO₂.

Fig. 10 shows the profile of thiophene HDS conversion on $Co-TiC/SiO_2$ catalysts. $Co-TiC/SiO_2$ catalysts were pretreated with H₂ prior to use. Carburized Co/SiO₂ catalyst (without Ti) showed no activity toward thiophene HDS reaction. However, $Co-TiC/SiO_2$ showed the activity toward thiophene HDS reaction. It was found that reduced Co species show no activity, and that the activity of $Co-TiC/SiO_2$ depended on TiC.

The activity of Co–TiC/SiO₂ treated with H₂ at 1073 K was greater than that of Co–TiC/SiO₂ treated with H₂ at 773 K. Such results suggested that Ti-oxide and deposited carbon species coated on the surface of TiC were removed by high temperature hydrogen treatment. The activity of sc Co–TiC/SiO₂ was greater than that of co Co–TiC/SiO₂. This trend was

similar to the carburization degree of TiC. It was found that the activity toward thiophene HDS reaction was related to the carburization degree of TiC for Co–TiC/SiO₂ catalysts. It was supposed that higher activity could be expected by further increase of the carburization degree.

4. Conclusion

- (1) Carburization temperature of Ti-oxide into TiC could be lowered down to 1173 K by addition of Co.
- (2) The formation of TiC is affected by carburization temperature rather than by retention time.
- (3) Co–Ti/SiO₂ was prepared by use of successive impregnation method (sc) and co-impregnation method (co). Carburization degree of sc Co–TiC/SiO₂ was deeper than that of co Co–TiC/SiO₂.
- (4) The activity toward thiophene HDS reaction on sc Co–TiC/ SiO₂ was greater than that of co Co–TiC/SiO₂.

Acknowledgments

The present work is supported by the Grant-in-Aid for Scientific Research (KAKENHI) in Priority Area "Molecular Nano Dynamics" from the Ministry of Education, Culture, Sports, Science and Technology (No. 17034011).

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