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Cite this: *RSC Adv.*, 2015, 5, 61410

Effective removal of methylene blue from water using phosphoric acid based geopolymers: synthesis, characterizations and adsorption studies

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Phosphoric acid based geopolymers (PAGPs) are a class of geopolymers that are produced by phosphoric acid activation of metakaolin. In this work, two different PAGPs have been synthesized using phosphoric acid to alumina molar ratios of 1:1 and 1.2:1. The surface profile, chemical composition, micromorphology, and texture properties of the geopolymers were instrumentally determined. Both geopolymers have shown a mesoporous profile with the avg. pore size of 8.6 and 19.4 nm by GP-1M (P : Al = 1 : 1) and GP-2M (P : Al = 1.2 : 1), respectively. Thermogravimetric analysis revealed that these geopolymers were thermally stable up to 800 °C, although the formation of quartz, cristobalite and tridymite was observed in XRD analysis of the samples treated at 800 °C for two hours. The synthesized geopolymers were utilized for the adsorption of methylene blue (MB) by investigating the effect of the amount of adsorbent, pH of the solution and shaking period. The batch kinetics study fitted best into the pseudo second order (PSO) reaction kinetic model. In isotherm modelling studies, the Langmuir isotherm model was best fitted and was used to describe the mechanism of the adsorption. Experimental adsorption capacities (q_e) of 2.84 and 3.01 mg g⁻¹ were recorded for GP-1M and GP-2M, respectively. Used adsorbents were successfully regenerated by furnace treatment at 400 °C for two hours, and the regenerated adsorbents presented enhanced adsorption capacities in the range of 4.9–5.07 mg g⁻¹ for five repeat cycles, elucidating that the material is suitable for multiple time use.

Received 5th May 2015

Accepted 9th July 2015

DOI: 10.1039/c5ra08255b

www.rsc.org/advances

Introduction

The existence of colorants in wastewater is considered as a major environmental issue due their impact on the environment and life. Owing to the increasing industrialization in the textile, paper, plastics, leather, manufacture and furniture sectors, the utilization of dyes is growing day by day.¹ Approximately 0.7 million tonnes of different types of dyes (~0.1 million varieties) are produced every year.² The colour of water is considered as an important parameter that indicates the quality of the water, as the presence of a minute quantity of dye is readily observable. Most of the dyes are large organic molecules; therefore they offer serious threats to the marine and inland life, and the environment. Methylene blue (MB) is among the most commonly used dyes in the fabrics and furniture industries. The occurrence of MB in the effluent water can cause permanent blindness, asthma and abdominal disorders like vomiting, nausea *etc.* Owing to the health and ecological issues, MB removal from water effluents is needed.^{3,4}

Removal of dyes from wastewater is achieved by applying a variety of methods including, adsorption, photodegradation,

ultrafiltration, ion exchange, electrochemical and sonochemical degradation, and reverse osmosis *etc.*⁵ Due to the complex treatment protocols, high expenses, and the large volumes of contaminated water, the water treatment scenario became more complicated. Finding of new, cheap and simple materials and methods are necessarily needed for wastewater treatment.¹ Adsorption is considered as one of the most effective techniques for the wastewater treatment due to the existence of a number of adsorbent materials having low cost, ready availability and can be fabricated using simple synthesis protocols. Researchers have put their efforts to discover alternate materials having the ability to decontaminate wastewater.^{5,6}

Activated carbon is most widely used, as an adsorbent, for wastewater treatment and purification, owing to its higher porosity and ready availability.⁵ Other most commonly used adsorbents studied for the MB removal from wastewater include bio sorbents, wood, rice husk ash, zeolites, fly ash, chitosan, cellulose, kapok, cotton and geopolymers *etc.*^{7–9} Although, these materials have been successful in an effective removal of dyes from wastewater, but some of the issues still need to be addressed. Recycling and regeneration of the adsorbents is of utmost importance since it contributes to the sustainability of the process. Moreover, the thermal stability of the materials is another issue that needs to be addressed. Most

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of the organic type adsorbents are difficult to be recycled and re-used due to their thermal instability and solubility in organic solvents used for the recovery of MB. Easy recyclability and thermal stability up to 1000 °C made geopolymers as a choice adsorbent for waste water treatment.¹⁰

Geopolymers are the green materials prepared by the chemical interaction of raw source of aluminosilicates *e.g.* coal fly ash, calcined clays (metakaolin), and the slags from metallurgy, with an aqueous alkaline and/or alkaline silicate or phosphoric acid solutions as reaction process accelerators and inducing the development of solid, insoluble binding material. Davidovits, in 1970s, was first to introduce the term “geopolymer” for the alkali activated metakaolin. The products were commercialized as fire resistant, inorganic materials; he used the term “geopolymer” to highlight some of the resemblances of geopolymers with organic thermoset resins.^{11,12} Geopolymers have offered interesting applications, being having a diverse chemistry, zeolite like structure and properties, and their physical properties *e.g.* thermal and corrosion stability *etc.*^{13,14} Being porous in nature, geopolymers have been utilized as adsorbent materials and photocatalysts for the removal of heavy metals contaminations, organic dyes from wastewater, and adsorption of indoor formaldehyde. Adsorption capacities of alkali activated materials have been recorded several times higher than their starting precursor.⁵ Recently, a new class of geopolymers was prepared by phosphoric acid activation of metakaolin and was coined as phosphoric acid-based geopolymer (PAGP).^{15–18} PAGPs have offered interesting properties *e.g.* porosity and thermal stability *etc.*, which can make them suitable alternative for the waste water treatment. Adsorption properties of PAGPs have not been reported, to the best of our knowledge and owing to their reusability, thermal stability and regenerability, these polymers can play an important role in wastewater treatment.

In this study, PAGPs were synthesized using metakaolin as raw source of aluminosilicates and phosphoric acid as activator. PAGPs were investigated as recyclable and readily renewable adsorbents for the adsorption of MB. The objective of this work is to explore the suitability of PAGPs for the wastewater treatment application with an emphasis on kinetics and isothermal modelling.

Experimental

Materials

Kaolin and α -alumina (Al_2O_3) were procured from R&M chemicals and kaolin was used for the preparation of metakaolin. Phosphoric acid (85%, Merck Millipore) was used as activator in the synthesis of geopolymers and distilled water was used throughout the study. Methylene blue was obtained from R&M chemicals and a 500 mg L⁻¹ solution was prepared using demineralized water and was used as stock solution to prepare individual solutions. To prepare metakaolin, the raw kaolin was calcined in a furnace (Protherm, Turkey) at 800 °C for 2 hours.

To know the conversion temperature of kaolin to metakaolin, thermogravimetric analysis (TGA) of kaolin was carried out in a simultaneous thermal analyser (STA 6000, Perkin

Elmer) under nitrogen atmosphere, in the temperature range of 50–800 °C at a heating rate of 20 °C min⁻¹.

As shown in Fig. 1, 14.3% mass loss was occurred during metakaolinization and the TG, DTG and DTA patterns match with the previously reported literature, confirming that kaolin has been converted to metakaolin at 650 °C.^{19–21} To ensure the correct formulation and mix design of the geopolymers, kaolin and metakaolin were analysed using X-ray fluorescence spectrometry (XRF) and the results are shown in Table 1.

Methods

Preparation of geopolymers. The process of geopolymer synthesis is comprised of two steps; the mixing of the starting materials with phosphoric acid and the subsequent curing. In the first step, metakaolin was mechanically mixed with α - Al_2O_3 powder, and then phosphoric acid and distilled water were added to form a slurry mixture. Two mixtures with P : Al ratios of 1 : 1 (GP-1M) and 1.2 : 1 (GP-2M) were prepared in accordance with Table 2. The two different P : Al ratios were used to provide extra phosphate anions in the reaction, ensuring complete reaction among reactants. Both mixtures were evenly stirred for 30 minutes with a Teflon coated stirrer and were poured into covered plastic moulds. The moulded samples were cured in an oven at 80 °C for 12 hours. Dried and

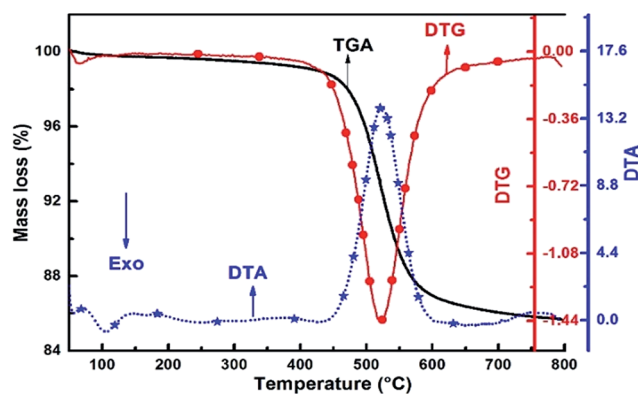


Fig. 1 Thermogravimetric analysis of the kaolin in N₂ environment. TG, DTG and DTA curves are shown in the figure.

Table 1 XRF analysis of kaolin and metakaolin

	Al ₂ O ₃	SiO ₂	P ₂ O ₅	TiO ₂	Fe ₂ O ₃	CaO	K ₂ O	Minor comp.
Kaolin	37.7	55.9	1.7	1.76	1.74	0.46	0.37	0.397
Metakaolin	38.9	55.4	1.6	1.65	1.47	0.43	0.35	0.173

Table 2 Mix design for geopolymers preparation

Geopolymer	Metakaolin	α -Aluminum oxide (Al ₂ O ₃)	Phosphoric acid (H ₃ PO ₄)	Distilled water
GP-1M	50.00 g	38.82 g	31.96 cm ³	40.00 cm ³
GP-2M	50.00 g	38.82 g	38.35 cm ³	40.00 cm ³

cured samples were ball-milled into powder for characterization and adsorption tests.

Characterization of geopolymers. Particle size distribution of the geopolymers was determined using the particle size analyser (Mastersizer 2000, Malvern). Pore size distribution and surface properties of the geopolymers were determined by Mercury Intrusion Porosimetry (MIP). Prior to analysis, geopolymers were cut into the dimension of $\approx 8 \text{ mm} \times 8 \text{ mm} \times 10 \text{ mm}$, and the density of geopolymers were determined using pycnometer (Quanta chrome, Ultra Pycnometer 1000). Additionally, the surface area, avg. pore size and pore volume of the geopolymers were determined using surface area and porosity analyser (ASAP, 2020, Micromeritics) using degassing temperature of $200 \text{ }^\circ\text{C}$.

The micromorphology of the geopolymers was studied with the aid of field emission scanning electron microscope (FESEM, Zeiss supra, Germany), at a magnification of $5000\times$. Powdered samples were mounted on the aluminium stub using carbon tape and were analysed using secondary electron method. The chemical composition of the PAGPs was determined using Energy dispersive X-ray (EDX) coupled with the FESEM and were verified using X-ray Fluorescence (XRF, Bruker, Germany).

Thermogravimetric analysis of the geopolymers were conducted in thermogravimetric analyser (STA 7000, Perkin Elmer) in the temperature range of $50\text{--}800 \text{ }^\circ\text{C}$, at a heating rate of $10 \text{ }^\circ\text{C min}^{-1}$ and under N_2 environment (20 mL min^{-1}).

To investigate the crystallinity and amorphousity of the powdered geopolymers, X-ray diffraction (XRD) analysis was carried out on an X-ray diffractometer (D8 Advanced, Bruker, Germany), in the 2θ range of $2\text{--}80^\circ$.

Adsorption tests. Adsorption tests were conducted using methylene blue stock solution (500 mg L^{-1}). The stock solution was diluted to 10, 30 and 50 mg L^{-1} for the adsorption tests. Table 3 shows the summary of experimental design for the adsorption tests. Details of the adsorption test are given in the next sections.

Effect of adsorbent dosage. The effect of adsorbent dose on the adsorption of MB was investigated by adding varying quantities of geopolymer (0.2, 0.4, 0.6, 0.8 and 1.0 g) into the flask having 25 mL of MB solution (50 mg L^{-1}) at normal pH at $28 \text{ }^\circ\text{C}$. The samples were shaken continuously at 150 rpm for 3 hours and the adsorbent was centrifuged out of the MB solution using a centrifuge (Biofuge, Thermo scientific, US), at 6000 rpm for 5 minutes. UV-Vis spectrophotometer (Shimadzu, double beam, UV1800, Japan) was used to determine the MB concentration in

the spectrophotometric mode. The removal of the dye (%) was calculated using eqn (1).

$$\text{Percent removal of dye} = \frac{C_0 - C_e}{C_0} \times 100 \quad (1)$$

where, the starting and equilibrium concentrations of the MB are represented by C_0 and C_e , respectively.

Effect of pH. To determine the effect of pH on the adsorption of MB, PAGPs (0.4 g) were mixed with 25 mL of MB (50 mg L^{-1}) solution at initial pH of 3, 5, 7, 9 and 10. MB solutions have an initial pH of 4.8, which were adjusted to the desired pH using sodium hydroxide (0.1 M) and hydrochloric acid (0.1 M) aqueous solution, and were confirmed by pH meter (S20, Mettler Toledo). The Dye solution was shaken in a water bath at $28 \text{ }^\circ\text{C}$, at 150 rpm for 180 minutes.

The extent of adsorption at equilibrium (q_{eq}) was determined using eqn (2).

$$q_{\text{eq}} = \frac{(C_0 - C_e)V}{M} \quad (2)$$

where, V and M represent the volume (L) of MB solution and amount of adsorbent (g), respectively.

Effect of contact time. To study the influence of contact period and to find the equilibrium time, batch adsorption kinetics was carried out. In this experiment, 0.4 g of adsorbent was mixed with 25 mL each of 10, 30 and 50 mg L^{-1} of MB solutions and the solutions were shaken for 180 minutes at $28 \text{ }^\circ\text{C}$. Samples were taken from the solution at 30, 60, 90, 120, 150 and 180 minutes intervals and were analysed with UV-Vis spectrophotometer. Adsorption capacities at a specific time q_t (mg g^{-1}) were computed using eqn (3).

$$q_t = \frac{(C_0 - C_t)V}{M} \quad (3)$$

where, " C_t " represents the MB concentration at a specific time " t ".

Batch kinetics studies. Lagergren pseudo first order (PFO) and type one pseudo second order (PSO) models were used to study the kinetics of the adsorption of methylene blue on PAGPs. Eqn (4) and (5) represent PFO and PSO models, respectively.²²

$$\log(q_{\text{eq}} - q_t) = \log q_e - \left(\frac{k_1}{2.303}\right)t \quad (4)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \left(\frac{1}{q_e}\right)t \quad (5)$$

q_e shows adsorption capacity (calculated) whereas pseudo-first-order and pseudo-second order adsorption rate constants are symbolised by k_1 (min^{-1}) and k_2 ($\text{g mg}^{-1} \text{ min}^{-1}$), respectively. The value of q_e is calculated from the intercept of the $\log(q_{\text{eq}} - q_t)$ vs. t using eqn (4) and from the slope of the t/q_t vs. t using eqn (5).

Isotherm models studies. Three different isotherm models *i.e.* Langmuir, Freundlich and Temkin models were applied to describe the interactions of MB with geopolymers and are shown in eqn (6)–(8), respectively.^{23–25}

Table 3 Experimental design for adsorption test

Investigated parameter	Initial conc. (mg L^{-1})	PAGP dose	pH	Contact time/min
Dose	50	0.2, 0.4, 0.6, 0.8, 1.0	4.8	180
pH	50	0.4	3, 5, 7, 9, 10	180
Contact time	10, 30, 50	0.4	4.8	30, 60, 90, 120, 150, 180

$$\frac{1}{q_e} = \frac{1}{q_m K_L} \left(\frac{1}{C_e} \right) + \frac{1}{q_m} \quad (6)$$

In eqn (6), adsorption capacity and energy of adsorption are represented by the Langmuir constants q_m (mg g^{-1}) and K_L (L mg^{-1}), respectively and their values can be calculated from the plot between $1/q_e$ versus $1/C_e$ according to eqn (6).

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e \quad (7)$$

K_F and “ n ” in eqn (7) are the Freundlich isotherm constants *i.e.* the measures of adsorption capacity and adsorption intensity, respectively. These values are calculated from the plot of $\ln(q_e)$ versus $\ln(C_e)$ using eqn (7).

$$q_e = B \ln A + B \ln C_e \quad (8)$$

where B and A represent the Temkin isotherm constant associated to the heat of sorption (J mol^{-1}) and Temkin isotherm constant (L g^{-1}), whereas R is the gas constant ($8.314 \text{ J mol}^{-1} \text{ K}^{-1}$). The values of A and B are obtained from the intercept and slope of the linear plot of q_e versus $\ln(C_e)$ using eqn (8).

Regeneration and re-use of the adsorbent. Used PAGPs were regenerated by heating in a furnace (Protherm, Turkey) at 400°C for 2 hours and were reused. To check the adsorption efficiency, 0.4 g of the adsorbent was added to 50 mL of MB solution (50 mg L^{-1}) and was stirred at 150 rpm at 28°C for 180 minutes. PAGPs were regenerated and reused for 5 times to investigate their re-utilization.

Results and discussion

Characterization of materials

Physical properties of geopolymers. Physical properties of the geopolymers are listed in Table 4. Both geopolymers have approximately similar physical properties. Particle size distribution analysis is considered as an important property. Although the mean particle size of GP-2M is slightly smaller than GP-1M (4.20 vs. $4.89 \mu\text{m}$), but the average surface area determined by mercury intrusion porosimetry are nearly alike. GP-1M has a surface area of $2.24 \text{ m}^2 \text{ g}^{-1}$, whereas GP-2M produced a surface area of $2.28 \text{ m}^2 \text{ g}^{-1}$.

On the other hand the avg. pore size, as determined by MIP, of GP-2M is 198 nm which is smaller than that of GP-1M *i.e.* 238 nm. The smaller pore size of GP-2M was caused by the extra phosphoric acid, leading to the formation of more compact

Table 4 Physical properties of GP-1M and GP-2M

Property	GP-1M	GP-2M
Density	2.33 g cm^{-3}	2.35 g cm^{-3}
Mean particle size (D_{50})	$4.89 \mu\text{m}$	$4.20 \mu\text{m}$
Surface area ^a	$2.24 \text{ m}^2 \text{ g}^{-1}$	$2.28 \text{ m}^2 \text{ g}^{-1}$
Pore size (avg.) ^a	238.0 nm	198.33 nm
Pore volume ^a	$133.5 \text{ mm}^3 \text{ g}^{-1}$	$113.09 \text{ mm}^3 \text{ g}^{-1}$

^a All these parameters were determined using MIP.

structure, as demonstrated in the increased density of the same sample. The supposition is further supported by the lower pore volume of GP-2M ($113.09 \text{ mm}^3 \text{ g}^{-1}$) compared to GP-1M ($133.5 \text{ mm}^3 \text{ g}^{-1}$).

As these geopolymers were cured in a sealed environment, therefore the increased quantity of phosphate anion (PO_4^{3-}) reacted with α -alumina and the aluminosilicates in the Meta-kaolin, leading to the formation of a denser geopolymer. The structure and properties of geopolymers vary with the composition of raw materials, concentration of activating solutions and curing conditions. Higher concentration of activators results in the formation of a denser geopolymer, primarily due to more reaction products, and secondarily due to the incorporation of more material in the geopolymer matrix.²⁶

Surface and pore profile. The surface profile of the PAGPs was tested using N_2 adsorption–desorption isotherms and the results are shown in Table 5 and Fig. 2. The BET surface area of the geopolymer samples was retrieved to be 33.39 and $8.807 \text{ m}^2 \text{ g}^{-1}$ for GP-1M and GP-2M, respectively. Both samples have displayed a characteristic type IV nitrogen adsorption–

Table 5 Textural parameters of PAGPS using BET analysis

Sample	Surface area (BET) ($\text{m}^2 \text{ g}^{-1}$)	Avg. pore diameter (nm)	Pore volume ($\text{cm}^3 \text{ g}^{-1}$)
GP-1M	33.39	8.61	0.071
GP-2M	8.07	19.43	0.035

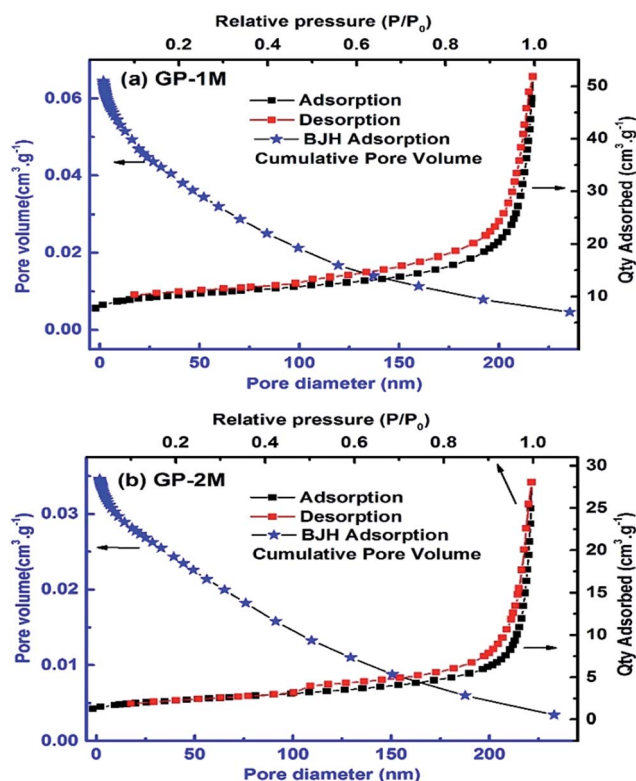


Fig. 2 Nitrogen adsorption–desorption isotherm and pore analysis profile of (a) GP-1M and (b) GP-2M.

desorption isotherm in accordance with the IUPAC scheme of classification, as shown in Fig. 2 (black and red lines).²⁷ Hysteresis loop in the P/P_0 range of 0.7–0.9 denotes the presence of mesopores (pores in the range of 2–50 nm).²⁸ The slight variation in the N_2 adsorption-desorption isotherms from standard type IV isotherm could be related to the existence of hetero sized pores. Moreover, the symmetry of the isotherm and hysteresis loop in geopolymers are affected by the nature of sample, degassing temperature and curing conditions.²⁹

Moreover, the Barrett-Joyner-Halenda (BJH) pore size distribution curves (blue line in Fig. 2) indicates that most of the pores are mesopores (2–50 nm), in both samples along with certain amount of micro (<2 nm) and macropores (>50 nm). The results demonstrated that PAGPs are consisted of various type of pores including micro, meso and macropores. The avg. pore size of the GP-1M and GP-2M was found to be 8.61 and 19.4 nm, respectively. Additionally, GP-1M has shown a cumulative pore volume of 0.071 that was nearly two fold to the pore volume of GP-2M.

The higher surface area of GP-1M is related to the small sized mesopores and the higher pore volume compared to GP-2M. The lower pore volume of GP-2M further strengthened the supposition that GP-2M has a compact texture with lesser porosity and the result is in consistence with the physical properties of PAGPs as discussed in previous section.

Methylene blue is a large molecule (approximately 0.8 nm) and is better adsorbed by mesoporous materials compared to microporous and macroporous materials.³⁰ The results demonstrated that with an increase in P : Al ratio, there was a subsequent decrease in porosity of PAGPs and the result is in agreement with MIP based surface analysis given in Table 4. Similar trend in results was also observed by other researchers.³¹

Microscopic studies. Scanning electron microscope (SEM) is utilized to investigate the micromorphology of the adsorbent materials. The FESEM micrographs of GP-1M and GP-2M are shown in Fig. 3(a) and (b), respectively. Both samples have shown amorphous texture, and the formation of zeolite like crystalline microstructures was not observed. In a closer examination, it is evident that the layered structure of meta-kaolin is absent in both samples, which is confirming the formation of geopolymers and the reaction between metakaolin and phosphoric acid. Two types of pores were observed in both samples; the larger pores (inter particle voids) in the range of 0.5–2 μm and the smaller pores below 0.5 μm . These pores provide channels for the adsorption of MB and facilitate the adsorption process. PAGPs are composed of considerable amount of larger pores.

The microstructure of GP-1M and GP-2M closely resembles to the typical amorphous morphology of the geopolymeric gel. Morphologies of different shapes and sizes were present in the microstructures. Geopolymers have shown multi morphologies and anisotropy due to the non-stoichiometric reactions, physically and chemically varying particles, and presence of crystalline phases in the raw materials.^{13,14,32}

Elemental composition of the two polymers was determined using EDX analysis and the results are given in Table 6. The

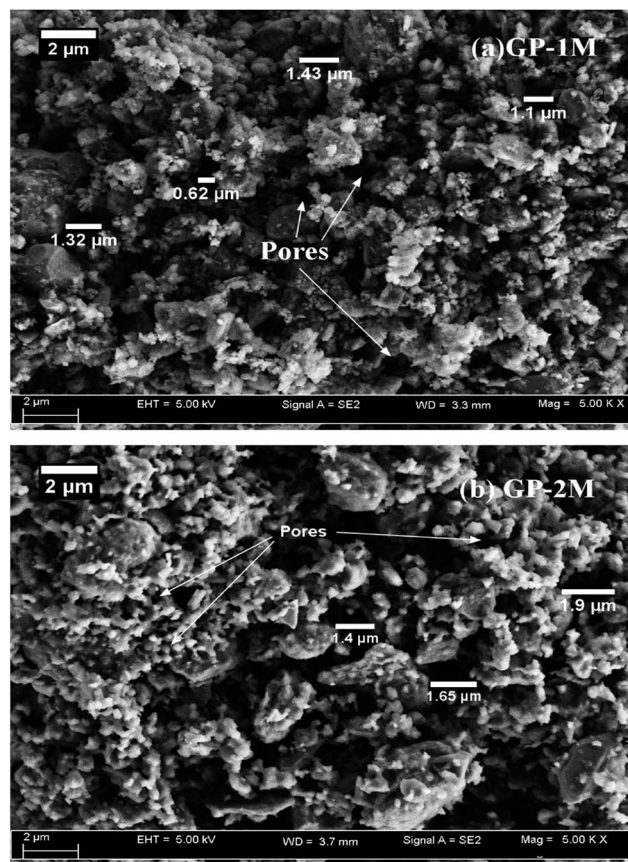


Fig. 3 FESEM analysis of (a) GP-1M and (b) GP-2M.

results show that GP-2M has 3% more phosphorus than GP-1M, due to the addition of extra phosphoric acid. Besides, an increase in Al content from 19.8% to 22.2% was also observed. This increase shows that with the addition of extra phosphoric acid, more active aluminium is available at the surface of the geopolymer. To verify that whether the change in aluminium content was a local phenomenon or it was distributed over the whole sample, XRF analysis was carried out.

XRF analysis of geopolymers. XRF analysis is considered as a more reliable technique compared to SEM-EDX, for the determination of the chemical composition of the materials. The

Table 6 EDX analysis of the geopolymers

Composition	O(K)	Al(K)	Si(K)	P(K)
GP-1M	59.43	19.84	9.78	10.94
GP-2M	55.04	22.26	9.64	13.06

Table 7 Chemical composition of GP-1M and GP-2M using XRF

	Al ₂ O ₃	SiO ₂	P ₂ O ₅	TiO ₂	Fe ₂ O ₃	CaO	K ₂ O	Minor comp.
GP-1M	36.5	26	35.1	0.75	0.75	0.46	0.19	0.253
GP-2M	34.2	24.3	39.3	0.72	0.69	0.43	0.14	0.315

chemical analyses of the two PAGPs are given in Table 7. Both samples are composed of SiO_2 , Al_2O_3 and P_2O_5 as principal components, along with trace amounts of other oxides. The increased P_2O_5 content in GP-2M can be observed compared to GP-1M and the result is consistent with the experimental design and previously discussed SEM-EDX analysis. Silica and alumina contents of the two samples show minor variations, representing that the difference observed in the SEM-EDX results were due to the distribution of aluminium on the surface of the geopolymers. The chemical composition of the geopolymers is not homogenous and different areas have different chemical compositions. Anisotropy in chemical composition of geopolymer is previously reported and is caused by the multiple components in the starting material, reaction conditions and material processing protocols.³³

The major difference between alkali based and phosphoric acid based geopolymers is that the former are formed of alkali metal aluminosilicates, whereas the later are silico aluminophosphates. Phosphoric acid activates metakaolin by providing low-polymeric $(\text{PO}_4)^{3-}$ tetrahedral species and leading to the formation of three dimensional silico aluminophosphates.^{34,35}

Thermal stability of the geopolymers. Thermal stability of the adsorbents is prerequisite for their regeneration and reutilization. Thermogravimetric analysis was used to investigate the thermal stability of PAGPs and the results are given in Fig. 4(a) and (b). Both samples have shown identical thermal behaviour and revealed a thermal stability up to 800 °C, under nitrogen environment. A total of 9.5 and 9.2% mass loss was

observed for the GP-1M and GP-2M, respectively. Approximately 8% of the mass loss is below 200 °C, represented by a sharp and well defined DTG peak at 110 °C.

The mass loss shown below 200 °C is accounted for the dehydration of the geopolymer, as water molecules are vaporized in this region, as reported previously.^{10,36} The results demonstrated that PAGPs are thermally stable and resist any thermal decomposition up to 800 °C. Moreover, it is also confirmed that the addition of extra phosphate ions have no impact on the thermal stability of the PAGPs.

Previous studies suggested that geopolymers are thermally very stable and only dehydration takes place up to 800 °C.¹⁰ This higher thermal stability is given by the stable silico aluminophosphate and aluminosilicate type structure.^{10,34} Liu *et al.* reported a mass loss of approximately 16% with a single DTG peak at 139 °C, representing the water loss during thermogravimetric analysis.¹⁶ The reduced water content of the PAGPs, in this study, was due to the addition of less water during synthesis of geopolymers.

It is concluded that these geopolymers can be readily regenerated by sintering the spent PAGPs. To confirm the regeneration and reusability of the used geopolymers, rejuvenated geopolymers were also investigated for the adsorption process. To investigate the effect of thermal treatment on the crystallinity of geopolymers, XRD analysis was carried out and is discussed in next section.

X-ray diffraction studies. X-ray diffraction analysis provides an insight of the various crystalline phases and amorphous content present in the geopolymers. The XRD patterns of the original (GP-1M and GP-2M), thermally treated (GP-1MT, GP-2MT) and regenerated (GP-1MR and GP-2MR) samples are shown in Fig. 5(a) and (b). Original geopolymers exhibited typical background hump in the 2θ range of 20–30°, associated with a typical amorphous geopolymers. The peaks at $2\theta = 25.584^\circ, 35.13^\circ, 37.78^\circ, 43.36^\circ, 52.55^\circ, 57.52^\circ,$ and 68.19° in all samples matched with diffraction pattern of α -alumina (ICOD card no. 00-010-0173), showing the presence of unreacted α -alumina. The intensity of these peaks are higher in GP-1M compared to GP-2M, showing that the higher phosphoric acid content resulted in dissolution of more α -alumina. The result is consistent with the BET and FESEM analysis discussed earlier showing that more geopolymer has been formed in GP-2M.

Geopolymers calcined at 800 °C for 2 hours are represented by GP-1MT and GP-2MT. As illustrated in Fig. 5(b), thermal treatment resulted in the formation of three new peaks in the 2θ range of 20–30°; the region representing the amorphousness of geopolymers. These new peaks were resulted due to the formation of quartzite, cristobalite and tridymite type structures.^{34,37} This behaviour of PAGPs is explained on the basis of partial transformation from amorphous to crystalline structure owing to the thermal treatment. Quartzite and cristobalite formation is caused either by the conversion of the unreacted amorphous silica, or due to transformation of silico aluminophosphate type structure. In the previous works, the formation of quartz, cristobalite and tridymite occurred at temperature ≈ 700 °C in the phosphoric acid activated metakaolin.

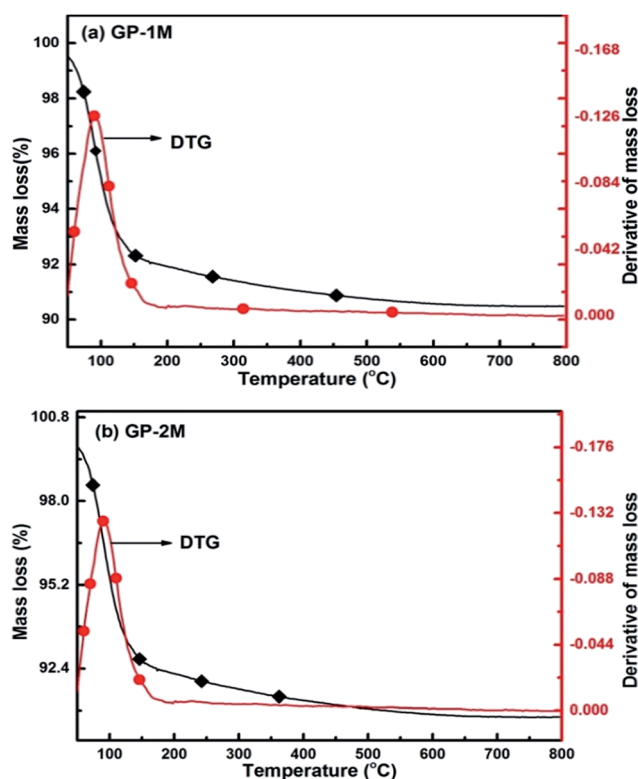


Fig. 4 Thermogravimetric analysis of (a) GP-1M and (b) GP-2M in N_2 environment.

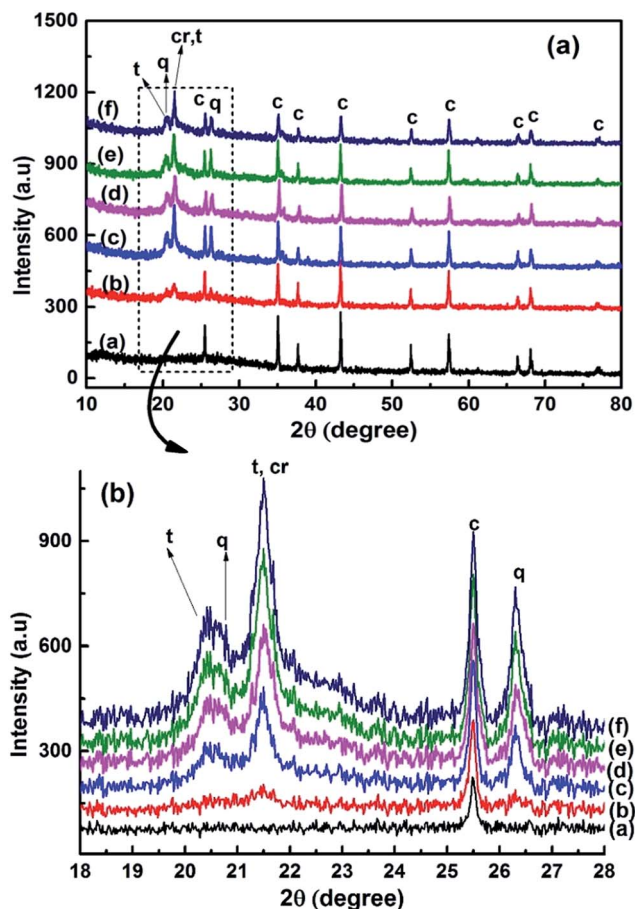


Fig. 5 (a) XRD analysis of the PAGPs and (b) a closer view of the selected region. In the figure samples details are; (a) GP-1M, (b) GP-2M, (c) GP-1MT (d), GP-2MT (e) GP-1MR and (f) GP-2MR, whereas "T" represents samples treated at 800 °C for 2 hours and "R" stands for regenerated adsorbents. Small letter c, cr, t and q are used to represent corundum, cristobalite, tridymite and quartzite phases.

The XRD pattern of the regenerated PAGPs closely resembled with the thermally treated ones in the 2θ range of 20–30°. This shows that formation of crystalline phases from amorphous geopolymers occurred as a result of heating the samples even at 400 °C, for two hours. The presence of crystalline phases can be linked with the longer thermal treatment compared to previously reported results.³⁴ Liu *et al.* investigated the thermal stability and crystallinity of phosphoric acid geopolymers up to 1500 °C and found that despite the changes in crystallinity of the geopolymers with the thermal treatment, there is no effect on their thermal stability and porosity.¹⁶

Adsorption of methylene blue

To explore the adsorption properties of GP-1M and GP-2M, adsorption tests were performed using methylene blue solution. The details of the studies are discussed in the next sections.

Effect of initial adsorbent dosage. Effect of adsorbent dose on the adsorption of MB was determined to find the optimum dose of the adsorbent. Fig. 6(a) represents the removal (%) of

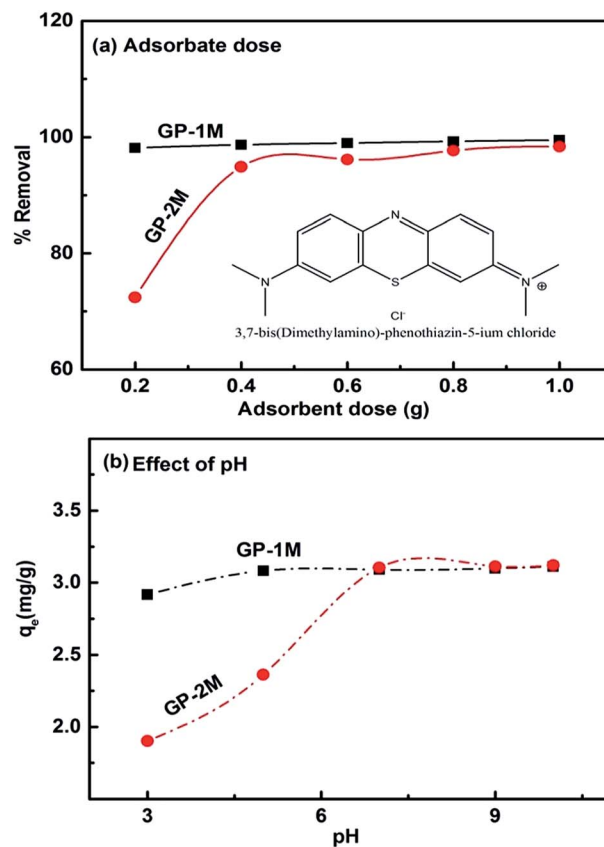


Fig. 6 (a) Effect of the initial adsorbent dosage and (b) pH on methylene blue adsorption using GP-1M and GP-2M. Experiments were conducted at 28 °C using 25 mL of 50 mg L⁻¹ MB solution.

MB by GP-1M and GP-2M at different adsorbent dosage. It is obvious from the Fig. 6(a), that the adsorption efficiency of GP-2M rises with the increase in adsorbent dose, whereas the GP-1M has removed most of the dye even at the lowest dose of 0.2 g. In case of GP-2M, beyond 0.4 g there is no visible increase in the dye removal and this dosage is considered as optimum and was used in the rest of the experiments. Moreover, the results also showed that the adsorption activity of GP-1M and GP-2M are approximately similar at a higher dosage, showing that there is no considerable effect of phosphorus content on the dye removal.

The higher adsorption capacity of GP-1M at lower adsorbent dosage is due to the higher surface and pore volume of GP-1M.

The rise in the dye adsorption with the increase in adsorbent dosage occurred due to the availability of more surface area and pores, owing to the presence of more adsorbent. Similar trend is being tracked in most of the previous literature related to the dye removal.^{38–41}

Effect of pH. pH is considered as an important factor that is affecting the adsorption efficiency of the geopolymers and other adsorbents. In this study, five different pH values *i.e.* 3, 5, 7, 9, and 10 have been scrutinized and the results are shown in Fig. 6(b). The results showed that the adsorption power of both geopolymers increased with the gradual increase in pH, from pH 3 onwards and the maximum adsorption was attained at pH

10. Although, GP-1M and GP-2M have shown differences in adsorption capacities, especially in the acidic pH, but both samples showed similar adsorption profiles at neutral and basic pH. The variation in MB adsorption at lower pH is attributed to the higher surface area and enhanced porosity of the GP-1M. The presence of more mesopores resulted in the increased adsorption by GP-1M.

The findings are similar to previous studies as methylene blue is a cationic dye and its adsorption is favoured at basic pH. From the observation, we can deduce that an acidic condition is unfavourable for the adsorption activities of geopolymers.^{41,42}

Effect of contact time. Adsorption of dyes varies with change in initial conc. of dyes and contact time. Results of the effect of initial dye concentration (10, 30 and 50 mg L⁻¹) and contact time (30–180 min) on adsorption of MB upon GP-1M and GP-2M are shown in Fig. 7(a) and (b). The results showed that the adsorption process is very fast and most of the dye is adsorbed in the first 30 minutes, whereas the equilibrium was attained in 90 minutes by both adsorbents. This quicker adsorption can be related to the availability of the free adsorption sites at the start of the process where the dye was being adsorbed. After saturation of the available sites, there was no further adsorption and the equilibrium was attained. It is deduced from Fig. 7 that the adsorption capacity of the geopolymers increased with the increase in dye concentration; the maximum capacity is given

by 50 mg L⁻¹ solution. Furthermore, with the increase in dye conc., the equilibrium conc. (C_e) of the MB for 50 mg L⁻¹ solution was lesser than 30 mg L⁻¹ and 10 mg L⁻¹ solutions.

Necessary to mention that both GP-1M and GP-2M exhibited similar adsorption capacities of 2.84 and 3.01 mg g⁻¹, showing that extra phosphate has a negligible effect on adsorption properties of the geopolymers. Although the equilibrium was attained within first 90 minutes, but the process was extended up to 180 minutes to ensure the complete equilibrium. Most of the previous investigations have reported a similar behaviour of the adsorbents. The equilibrium time is specific for every material and most of the previous studies showed equilibrium time of 90–180 minutes. The equilibrium time is dependent on the surface area and porosity of the adsorbents.^{40,43}

Batch kinetics studies. The kinetic study of the adsorption of MB using GP-1M and GP-2M was observed by conducting the adsorption test under different initial concentrations of methylene blue and the samples were collected at 30 minutes interval over a period of 180 minutes. Experimental data was plotted using the pseudo-first order (PFO) and type 1 pseudo second order equations (PSO) for GP-1M and GP-2M, respectively. Fig. 8(a) and (b) represents the PFO kinetics (linear form) of MB removal using GP-1M and GP-2M, respectively. Results of the kinetics parameters obtained for PFO model are shown in Table 8. The extent of fitting (R^2) was used to determine the best

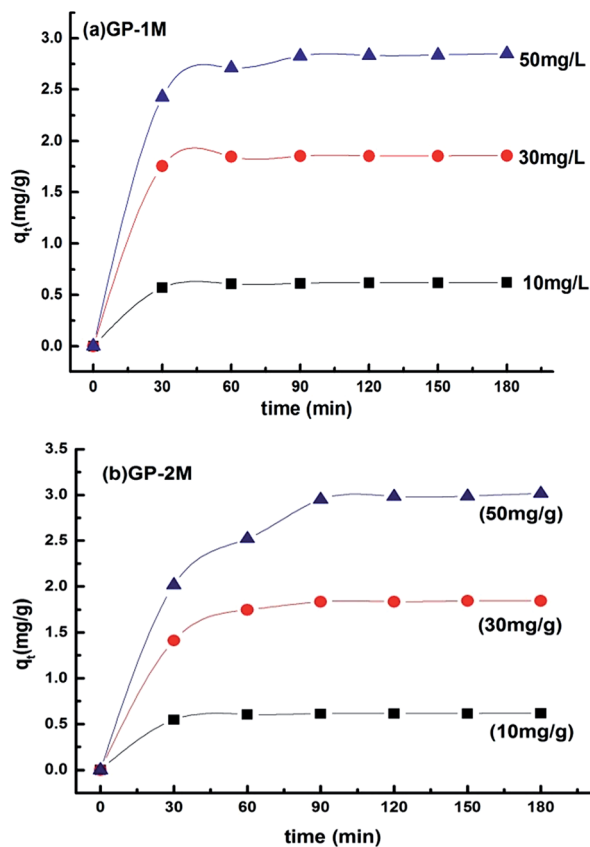


Fig. 7 Effect of initial conc. and time on the MB adsorption over (a) GP-1M and (b) GP-2M (25 mL of MB solution was used at 28 °C and 150 rpm).

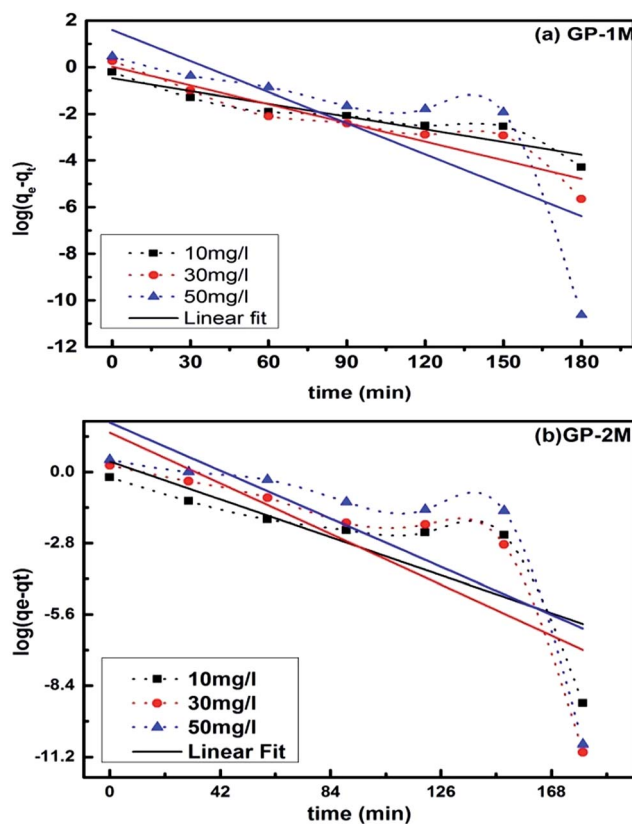


Fig. 8 Pseudo first order kinetics model (a) (GP-1M) and (b) GP-2M (25 mL of MB solution were used at 28 °C and 150 rpm).

Table 8 Comparison of PFO kinetics parameters of GP-1M and GP-2M

GP	C_0 (mg L ⁻¹)	k_1 (min ⁻¹)	$q_{e,cal}$ (mg g ⁻¹)	R^2
GP-1M	10	0.0419	0.3318	0.8674
	30	0.0615	1.0440	0.8619
	50	0.1022	39.4639	0.5133
GP-2M	10	0.0818	2.5887	0.5568
	30	0.1093	35.4446	0.5826
	50	0.1037	88.3609	0.4811

Table 9 Comparison of PSO kinetics parameters of GP-1M and GP-2M

GP	C_0 (mg L ⁻¹)	K_2 (g mg ⁻¹ min)	$q_{e,cal}$ (mg g ⁻¹)	R^2
GP-1M	10	0.6100	0.6297	1.000
	30	0.4015	1.8718	1.000
	50	0.0653	2.9418	1.000
GP-2M	10	0.4595	0.6306	1.000
	30	0.0623	1.9468	0.998
	50	0.0169	3.3553	0.996

model for MB batch kinetics. The R^2 values were found in the range of 0.48 for least fitted to 0.86 for best fitted results.

The adsorption capacities calculated using PFO model not only show very poor fitting in terms of R^2 , but also represents a major difference between experimental and calculated values of adsorption capacities. The results suggest that MB adsorption using PAGP did not follow PFO model. Most of the previous studies, using solid adsorbent, also deviated from PFO model.^{8,42}

As the PFO model is not followed by PAGPs, therefore pseudo second order (PSO) was used to determine the kinetics of MB adsorption on PAGPs. The plot of t/q_t vs. t (PSO model) for the batch kinetics of GP-1M and GP-2M is presented in Fig. 9. The

values of the rate constant (K_2), adsorption capacity (q_e) and R^2 are given in Table 9. The results show best fitting in the range of 0.996–1, showing that PSO model is adopted by MB adsorption on PAGPs. Moreover, the findings were further supported by the closeness between the adsorption capacities of PSO model and experimental data.

The results of the present study closely resemble with the previously reported ones. Most of the dye adsorptions on geopolymer, zeolites and fly ash follow PSO model.^{1,8,44,45} Azizian *et al.* explored the adsorption of MB on fly ash and concluded that at high initial conc. pseudo first order and at lower initial conc., pseudo second order is obeyed.⁴⁴ The increase in adsorption capacity with increase in initial conc. of dye suggests that MB conc. provides a driving force to the dye molecules to accumulate on the adsorbent surface.^{8,40}

Isotherm models studies. Isotherm study provides an insight of the association between the adsorbent's surface and the dye molecules. Three well-known models *i.e.* Langmuir, Freundlich and Temkin models were used in this study to investigate the isothermal adsorption of MB on PAGPs. Fig. 10(a)–(c) represents the Langmuir, Freundlich and Temkin isotherm models of GP-1M and GP-2M, respectively. The data of the isotherm parameters and the extent of fitting (R^2) of these isotherm models is tabulated in Table 10. The linear plot of $1/q_e$ vs. $1/C_e$, shown in Fig. 8(a), shows that MB adsorption on PAGPs follows Langmuir isotherm. The observation is further supported by the value of R^2 (0.996, 0.999 for GP-1M and GP-2M, respectively) and the adsorption capacity ($q_{e,cal}$), which are closer enough to adsorption capacities obtained from the experimental data and PSO model as well. The extent of fitting of Freundlich and Temkin models are lesser than Langmuir isotherm for both samples, showing that both samples have an approximately similar mechanism of adsorption. The best fitting of the Langmuir isotherm represents a uniform distribution of adsorption sites on the adsorbent surface, whereas each site is having a uniform activation energy of adsorption and enthalpy.^{8,38}

Langmuir parameters have been used to predict the interaction between dye molecules and adsorbent using eqn (9).

$$R_L = \frac{1}{(1 - K_L C_0)} \quad (9)$$

where, C_0 and K_L represents the initial conc. of MB (mg L⁻¹), and the Langmuir constant (L mg⁻¹), respectively.

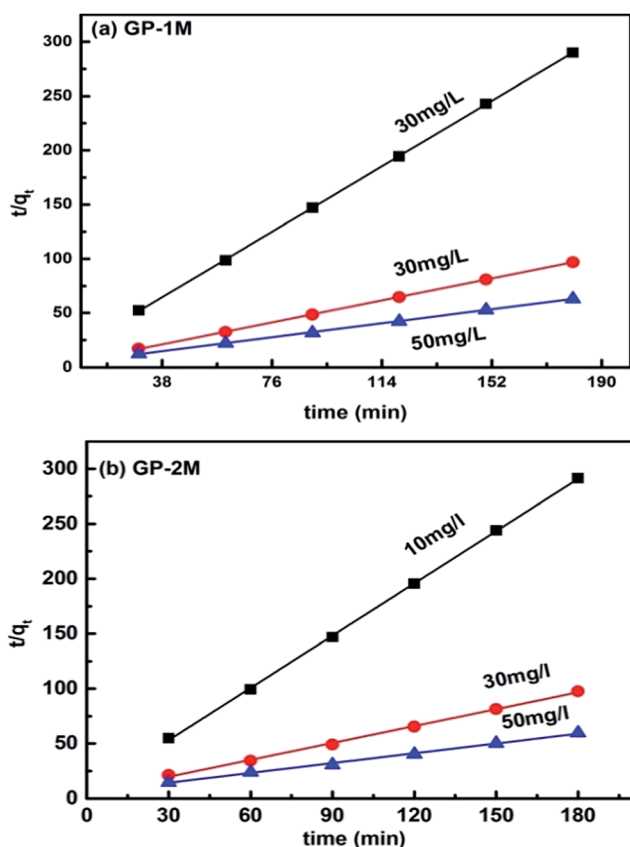


Fig. 9 Pseudo second order kinetics model of (a) GP-1M and (b) GP-2M (25 mL of MB solutions were used at 28 °C and 150 rpm).

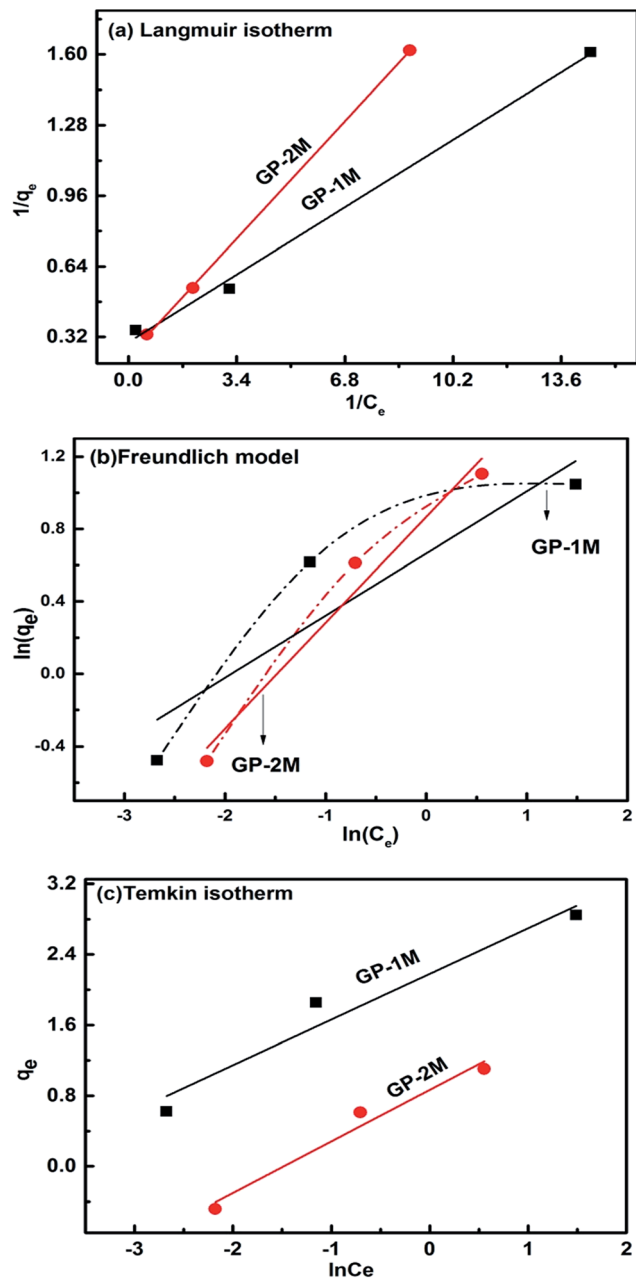


Fig. 10 Isotherm plots of GP-1M and GP-2M (a) Langmuir isotherm, (b) Freundlich isotherm and (c) Temkin isotherm.

Table 10 Isotherm parameters for MB adsorption on PAGP

Isotherm	Parameters	GP-1M	GP-2M
Langmuir	q_m (mg g^{-1})	3.371	4.260
	K_L (L mg^{-1})	3.299	1.503
	R_L	6.02×10^{-3}	1.31×10^{-2}
	R^2	0.996	0.999
Freundlich	n	2.912	1.705
	K_f	1.943	2.377
	R^2	0.694	0.968
Temkin	B	0.517	0.584
	A (L g^{-1})	67.467	4.399
	R^2	0.909	0.943

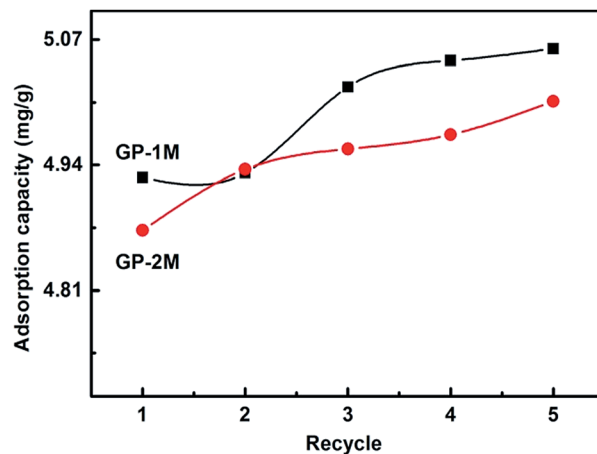


Fig. 11 Adsorption capacity of GP-1M and GP-2M after regeneration (50 mL of 50 mg L^{-1} MB solutions were used at 28°C and 150 rpm).

R_L represents a dimensionless separation factor that gives a check of the verification, if the adsorption in the system studied is unfavourable ($R_L > 1$), linear ($R_L = 1$), favourable ($0 < R_L < 1$), or irreversible ($R_L = 0$). The R_L values calculated for GP-1M and GP-2M are 6.02×10^{-3} and 1.31×10^{-2} , respectively; confirming that the adsorption process is favoured by these geopolymers. The increase in the value of R_L for GP-2M compared to GP-1M suggest that MB adsorption is reversible at higher phosphate level in these geopolymer and also leading to increased dye intake as shown by higher q_m value.^{5,8,38–40}

Regeneration and reuse of the adsorbent. Geopolymers were regenerated by the thermal treatment of spent adsorbents, and were reused for MB adsorption. Fig. 11 shows the adsorption capacities of the GP-1M and GP-2M after regeneration and reuse for 5 cycles. Noteworthy, the adsorption capacities of PAGPs increased from 2.84 to 4.92 mg g^{-1} for GP-1M and from 3.01 to 4.87 for GP-2M. Moreover, there was a gradual increase in adsorption capacities of PAGPs with increasing regeneration cycle for the five cycles.

This phenomenon is important as these geopolymers can be reused for several times by offering sustainability and industrial economy. This behaviour of geopolymers originated from the formation of new active surface sites due to the thermal treatment of PAGPs. As these polymers were cured at 80°C , therefore extra heating have led to the dehydration of bonded and interstitial water molecules, thus causing more active sites and increased porosity.¹⁰ The phenomenon can be further supported by the XRD analysis of regenerated PAGPs (Fig. 5). The existence of new phases may have resulted in the increased porosity and formation of new adsorption sites. Liu *et al.* observed the increase in porosity of PAGPs as a result of thermal treatment.¹⁶

Conclusion

Geopolymers were prepared by phosphoric acid activation of metakaolin and were characterized using different analytical techniques. These geopolymers are thermally unchanging and

consist of amorphous silico alumino phosphate structure. The amorphousness of PAGPS decreases with heating at 800 °C for 2 hours. The microstructure of these geopolymers is consisted of voids, macro and mesopores. PAGPs were studied as re-useable adsorbents for methylene blue removal. Methylene blue was successfully adsorbed on this new type of geopolymers and the maximum adsorption was achieved at pH 9 and 10. There was no effect of extra phosphoric acid on the adsorption properties of geopolymers, representing that P : Al = 1 is adequate for the synthesis of PAGPs. The process of adsorption followed Langmuir isotherm and pseudo second order kinetics. Geopolymers are thermally stable and have the ability to be regenerated using thermal activation. The material can be recycled for many times without any compromise on the adsorption properties. This new adsorbent has given a new window for methylene blue adsorption.

Acknowledgements

This work was supported by MOHE via FRGS grant no. 0153AB-i84.

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