# NUMERICAL INVESTIGATION OF COLLISION-INDUCED BREAKUP OF RAINDROPS. PART I: METHODOLOGY AS WELL AS DEPENDENCIES ON COLLISION ENERGY AND EXCENTRICITY 

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#### Abstract

Numerical investigations of binary raindrop collisions, comprising the drop pairs of Low and List (1982a), have been performed using a DNS tool based on the Volume-of-Fluid method. Looking at the coalescence efficiencies as well as the number and sizes of the fragment droplets, both agreement and discrepancies between the numerical simulations and the experimental data of Low and List (1982a) are observed. The results show that the size distribution of fragments is dependent on the collision energy and is shifted to smaller fragments for higher energies. In the second part of this paper, Straub et al. (2008) present new parameterizations of coalescence efficiencies and fragment size distributions based on the results obtained.


## 1 INTRODUCTION

Collision-induced breakup resulting from binary collisions of large raindrops is considered to be the principal mechanism limiting the size of raindrops (Pruppacher and Klett 1997). During this process, two raindrops that are moving at different velocities temporarily coalesce into one larger drop. The final outcome can be a single large raindrop or remnants of the original raindrops with a number of secondary droplets of different sizes. Comprehensive experimental investigations habe been presented in the past by Low and List (1982a) who, however, concentrated on very few drop pairs. Consequently the data base from which parameterizations have been derived is rather small and incomplete. Furthermore, the parameters relevant to this process like droplet velocity, droplet size, and most notably collision excentricity could not be determined with high accuracy. To overcome these deficiencies Beheng et al. (2006) have performed numerical experiments by computational simulations of binary collisions for same drop pairs as Low and List (1982a) and for some more drop pairs. The present study is a further extension of the work of Beheng et al. (2006) by again increasing the range of drop pair combinations and by additionally investigating the influence of excentricity and impact energy. To this end, the DNS-CFD code FS3D (Free Surface 3D) which has been developed at ITLR is applied. It solves the incompressible Navier-Stokes equations and employs
the Volume of Fluid (VOF) method to account for multiple phases. The free surface is reconstructed using the PLIC method and the convective transport is based on this reconstruction.

## 2 FORMULATION AND NUMERICAL METHOD

The applied code FS3D has been used for numerous investigations of drop dynamics in the past and is well validated. Gotaas et al. (2007) for example studied the effect of viscosity on binary droplet collisions, Rieber and Frohn (1999) simulated the process of drops splashing onto a liquid film.

### 2.1 Governing Equations

The representation of different phases is based on the Volume of Fluid (VOF) method by Hirt and Nichols (1981). In order to distinguish between the liquid and the gaseous phase, the additional field variable $f$ is introduced. $f$ is defined as

$$
f(\mathbf{x}, t)= \begin{cases}0 & \text { in the gaseous phase }  \tag{1}\\ 0<f<1 & \text { in cells containing a part } \\ & \text { of the interface } \\ 1 & \text { in the liquid phase }\end{cases}
$$

and is transported by

$$
\begin{equation*}
\frac{\partial f}{\partial t}+\nabla \cdot(f \mathbf{u})=0 \tag{2}
\end{equation*}
$$

In order to maintain a sharp interface, the convective transport of $f$ is performed based on the
reconstructed interface using the Piecewise Linear Interface Calculation (PLIC) method by Rider and Kothe (1998), thus minimizing numerical diffusion.

The governing balance equations for momentum read

$$
\left.\begin{array}{rl}
\frac{\partial(\rho \mathbf{u})}{\partial t}+\nabla \cdot & (\rho \mathbf{u}) \otimes \mathbf{u}
\end{array}\right)=-\nabla p+\rho \mathbf{k} .
$$

where $\mathbf{k}$ represents an external body force (e.g. gravity). The surface tension is included by the volume force $\mathbf{f}_{\gamma}$.
The continuity equation for the considered incompressible flow is given by

$$
\begin{equation*}
\nabla \cdot \mathbf{u}=0 \tag{4}
\end{equation*}
$$

The local fluid properties are obtained by applying the one-field formulation. Viscosity and density are hence calculated by

$$
\begin{align*}
\mu(\mathbf{x}, t) & =\mu_{l} f(\mathbf{x}, t)+(1-f(\mathbf{x}, t)) \mu_{g}  \tag{5}\\
\rho(\mathbf{x}, t) & =\rho_{l} f(\mathbf{x}, t)+(1-f(\mathbf{x}, t)) \rho_{g} \tag{6}
\end{align*}
$$

### 2.2 Spatial and Temporal Discretization

The spatial discretization of the equations is done using the Finite Volume method on a staggered grid and is of second order accuracy. The temporal integration is performed using the CrankNicholson method. A fast and robust multigrid solver is used for the projection of the velocity field onto one fulfilling eq. (4).

## 3 NUMERICAL SETUP AND SIMULATION PROCEDURE

All presented simulations were performed using a 3D computational domain with free-slip condition on the lateral walls and periodic boundary conditions on the bottom and top walls. This setup permits a numerically justifiable effort for the large number of conducted simulations as the collision process can be observed for a rather long time period using a limited computational grid. The spatial resolution was chosen to be $100 \mu \mathrm{~m}$ for all cases except investigations on grid dependency where a spatial resolution of $50 \mu \mathrm{~m}$ has been applied. According to the drops' sizes, different grids were employed, resulting in approx. $16 \times 10^{6}$ cells for the largest one $\left(2.56^{3} \mathrm{~cm}^{3}\right)$ used for standard calculations and nearly $135 \times 10^{6}$ cells for grid dependency investigations.

For the initial placement and velocities $v$ of the drops, terminal fall velocities have been calculated following Beard (1976). The vertical distance between the drops was set to $\Delta y=v \Delta t$ with $\Delta t=0.5 \mathrm{~ms}$, allowing for an interaction of the drops with their surrounding flow field to some extent. The nonspherical shape of large drops was


Figure 1: Numerical setup
considered by initializing them as ellipsoids with the ratio of the equatorial radii to the polar radius according to Beard and Chuang (1987). The excentricity of the droplet collisions, defined as the ratio of the distance of the drops' centers $\delta$ to the arithmetic mean of their diameters $d$ (with subscripts $L$ and $S$ for the large and the small drop, respectively)

$$
\begin{equation*}
\epsilon=\frac{2 \delta}{d_{L}+d_{S}} \tag{7}
\end{equation*}
$$

has been varied from 0.05 to 0.95 with six different excentricities ( $\epsilon=0.05,0.2,0.4,0.6,0.8,0.95$ ). The initial setup is sketched on a plane through the drops' centers in figure 1. Material properties for water and air were chosen at $20^{\circ} \mathrm{C}$ with a surface tension of $\sigma=73 \times 10^{-3} \mathrm{~N} / \mathrm{m}$.

The simulations were performed until a stable outcome of the collision process was reached. This condition was assumed to be fulfilled by a visual assessment of the results especially with the number of fragments becoming stationary. The number and size of the fragments were then determined by the use of a region growing approach. Mass conservation was satisfied for all cases. In order to compare to data from literature, the obtained results for different excentricities have been weighted according to their probability.

## 4 RESULTS

Overall, 32 drop pairs were investigated. Details of the drop diameters, the collision and surface energy and the resulting Weber number are given in table 1, an overview of the drop pairs considered is shown by figure 2. The 10 drop pairs investigated by Low and List (1982a) are included and listed as numbers 1-10 in table 1, those additionally simulated by Beheng et al. (2006) as 11-18; the remaining drop pairs (19-32) are considered to cover the pairs' matrix as complete as

| No. | $d_{L}$ | $d_{S}$ | $C K E$ | $S_{c}$ | $W e$ | No. | $d_{L}$ | $d_{S}$ | $C K E$ | $S_{c}$ | $W e$ |
| ---: | :--- | :--- | :--- | :--- | :--- | ---: | :--- | :--- | :--- | :--- | :--- |
| 1 | 0.18 | 0.04 | 0.33 | 0.75 | 0.44 | 17 | 0.32 | 0.04 | 0.73 | 2.35 | 0.31 |
| 2 | 0.4 | 0.04 | 0.86 | 3.67 | 0.23 | 18 | 0.41 | 0.14 | 9.6 | 3.96 | 2.43 |
| 3 | 0.44 | 0.04 | 0.9 | 4.44 | 0.2 | 19 | 0.24 | 0.06 | 1.29 | 1.33 | 0.97 |
| 4 | 0.18 | 0.07 | 0.92 | 0.77 | 1.19 | 20 | 0.3 | 0.07 | 2.43 | 2.08 | 1.17 |
| 5 | 0.18 | 0.1 | 0.99 | 0.83 | 1.2 | 21 | 0.36 | 0.07 | 2.97 | 2.99 | 0.99 |
| 6 | 0.3 | 0.1 | 4.18 | 2.11 | 1.98 | 22 | 0.45 | 0.07 | 3.43 | 4.66 | 0.74 |
| 7 | 0.36 | 0.1 | 5.46 | 3.01 | 1.81 | 23 | 0.12 | 0.1 | 0.07 | 0.45 | 0.15 |
| 8 | 0.46 | 0.1 | 6.62 | 4.89 | 1.35 | 24 | 0.41 | 0.1 | 6.18 | 3.89 | 1.59 |
| 9 | 0.36 | 0.18 | 8.55 | 3.21 | 2.66 | 25 | 0.25 | 0.12 | 3.14 | 1.54 | 2.04 |
| 10 | 0.46 | 0.18 | 12.53 | 5.04 | 2.48 | 26 | 0.3 | 0.12 | 5.04 | 2.15 | 2.34 |
| 11 | 0.06 | 0.04 | 0.01 | 0.09 | 0.12 | 27 | 0.36 | 0.12 | 6.93 | 3.05 | 2.28 |
| 12 | 0.12 | 0.04 | 0.12 | 0.34 | 0.35 | 28 | 0.46 | 0.12 | 8.7 | 4.91 | 1.77 |
| 13 | 0.12 | 0.06 | 0.24 | 0.36 | 0.68 | 29 | 0.36 | 0.14 | 8.07 | 3.09 | 2.61 |
| 14 | 0.25 | 0.04 | 0.55 | 1.44 | 0.38 | 30 | 0.18 | 0.16 | 0.13 | 1.06 | 0.12 |
| 15 | 0.24 | 0.09 | 2.36 | 1.37 | 1.73 | 31 | 0.41 | 0.16 | 10.62 | 4.01 | 2.65 |
| 16 | 0.27 | 0.15 | 3.93 | 1.86 | 2.11 | 32 | 0.25 | 0.18 | 1.88 | 1.77 | 1.06 |

Table 1: Investigated drop pairs, $d_{L}$ and $d_{S}$ in [cm], $C K E$ and $S_{c}$ in [ $\left.\mathrm{\mu J}\right]$


Figure 2: Investigated drop pairs; red squares indicate the pairs studied by Low and List (1982a).

## possible.

The collision energy of the drop pairs $C K E$ is calculated by ( $\rho_{l}=$ bulk density of water)

$$
\begin{equation*}
C K E=\frac{\pi}{12} \rho_{l} \frac{d_{L}^{3} d_{S}^{3}}{d_{L}^{3}+d_{S}^{3}}\left(v_{L}-v_{S}\right)^{2} \tag{8}
\end{equation*}
$$

the surface energy $S_{c}$ of the coalesced system is given by

$$
\begin{equation*}
S_{c}=\pi \sigma\left(d_{L}^{3}+d_{S}^{3}\right)^{2 / 3} \tag{9}
\end{equation*}
$$

The Weber number $W e$ is the ratio of the aforementioned energies

$$
\begin{equation*}
W e=\frac{C K E}{S_{c}} . \tag{10}
\end{equation*}
$$

### 4.1 Collision Outcomes

Results are shown exemplarily in figures 3 and 4 for two different drop pairs with 5 collision excentricities, respectively. The two pairs of drops chosen for this comparison have high (Pair 10, $C K E=12.53 \mu \mathrm{~J}$ ) and low (Pair 16, $C K E=3.93 \mu \mathrm{~J}$ ) collision energies.

For Pair 10 shown in figure 3 the dependency of the breakup mode on excentricity is evident. As it can be expected for the considered collision energy, there is disc breakup for $\epsilon=0.05$ and $\epsilon=0.2$, resulting in numerous small droplets of different sizes after the collision process. For $\epsilon=0.4$ and $\epsilon=0.6$, the breakup mode is sheet breakup and the size distribution of the secondary droplets is more homogeneous. For $\epsilon=0.8$ and $\epsilon=0.95$ (not shown), finally, there is filament breakup, the initial drops persist after the collision process with almost no change in drop size. Moreover some additional, very small droplets are produced. An overview on the mentioned dependency is also shown in figure 9 for the discussed droplet pair and two supplemental pairs with lower collision energies.

The collision outcomes for Pair 16 are shown in figure 4. For $\epsilon=0.05$ and $\epsilon=0.2$ the two drops form a single larger permanent drop after collison. For the other excentricities, there is filament breakup with no additional droplets for $\epsilon=0.4$ and $\epsilon=0.8$; some small secondary droplets are produced for $\epsilon=0.6$.

### 4.2 Budget of Energy

To get a picture of the evolution of energies during a collision process, the temporal development


Figure 3: Snapshots of droplet collisions at different times, Pair 10 ( $C K E=12.53 \mathrm{\mu J}$ )
of the kinetic energy of the fluid contained in the system, the surface energy and the surface area is depicted for Pair 26, $\epsilon=0.6$, in figure 5. Gravity was set to zero for this consideration. The appropriate images of the collision process are presented in figure 6. The surface energy is obtained as the product of surface area and surface tension. For convenience, both the initial surface energy and the initial kinetic energy are plotted starting from zero.
Looking at the surface area and energy, there is a sudden drop as the drops coalesce. This area reduction is caused by the contact of the two drops and the merging of their surfaces. Subsequently, the relative velocity leads to a strong deformation of the generated larger drop whereas the surface area is increased by about $50 \%$. That is followed by the separation into one large drop and several smaller droplets where the drops attain a roughly
spherical shape and oscillate.
The kinetic energy decreases at first during the aggregation phase of the drops. Then it increases again and reaches a momentary maximum as the liquid disintegrates and surface energy gets transformed. Subsequently, the kinetic energy is continuously reduced, presumably caused by viscous dissipation due to the inner flowfield of the drops and interaction with the surrounding gas.

### 4.3 Coalescence Efficiency

The coalescence efficiency $E_{c}$ is defined as the propability of coalescence for a binary collision process with a single drop resulting. For an experimental study consisting of numerous repetitions for one drop pair, $E_{c}$ is obtained by dividing the number of collisions leading to coalescence $c_{c}$ by


Figure 4: same as figure 3 but for Pair $16(C K E=3.93 \mu \mathrm{~J})$


Figure 5: Temporal evolution of kinetic energy, surface energy and surface area for drop pair $26, \epsilon=0.6$; left ordinate: surface area, right ordinate: energies
the total number of collisions $c$ :

$$
\begin{equation*}
E_{c}=c_{c} / c . \tag{11}
\end{equation*}
$$

It should be mentioned that an equipartition of collisions over the collision cross section (collision excentricities) is assumed for this approach. Keeping in mind the strong dependency of collision outcomes on excentricity, experimental results for $E_{c}$ seem to be quite sensitive to systematic errors influencing the aforementioned equipartition.

On the other hand, collisions with six different excentricities per drop pair were investigated numerically for the present study. Here, each collision is representing all collisions taking place in the according annulus of the projected collision cross section (circle with radius $r_{L}+r_{S}$ ). The result for one excentricity $\epsilon_{i}$ is weighted with the area of the corresponding annulus ( $\delta_{i}=$ separa-


Figure 6: Collision process of Pair 26, $\epsilon=0.6$


Figure 7: Coalescence efficiency vs. Weber number for all drop pairs. Numerically obtained results (stars) and values from the parameterization by Low and List (1982b) (circles)
tion distance, cf. figure 1)

$$
\begin{equation*}
A_{\odot, i}=2 \pi \delta_{i} \Delta \delta_{i}=2 \pi\left(r_{L}+r_{S}\right)^{2} \epsilon_{i} \Delta \epsilon_{i} \tag{12}
\end{equation*}
$$

Hence the coalescence efficiency is calculated by

$$
\begin{align*}
E_{c} & =\sum_{i c} A_{\odot, i c} / \sum_{i} A_{\odot, i} \\
& =\sum_{i c} \epsilon_{i c} \Delta \epsilon_{i c} / \sum_{i} \epsilon_{i} \Delta \epsilon_{i} \tag{13}
\end{align*}
$$

where $i c$ identifies excentricities for which coalescence occurs.

The results for the investigated drop pairs are plotted in figure 7 as function of the Weber number. Values obtained by the parameterization of Low and List (1982b) are shown additionally. Here, the agreement is quite good. Looking at the experimental values, there are several outliers with $E_{c}=0$ that do not seem physical; they are not reproduced by the numerical results. For small Weber numbers, the deviation between numerical
and experimental values is increasing. Whereas the coalescence efficiency of the simulations is approaching 1, the efficiency given by the Low and List parameterization is dropping to values of approximately 0.3 . This behaviour can be explained by the illegitimate application of the parameterization to the region of very low collision energies which has not been investigated by Low and List. For the numerical results on the other hand, the bouncing process taking place for very low relative velocities can not be simulated due to the employed numerical method, thus leading to values of $E_{c}$ which are too large.

### 4.4 Number of Fragments and Fragment Size Distribution

The mean number of fragments $\bar{n}$ is calculated analogously to the coalescence efficiency $E_{c}$ :

$$
\begin{equation*}
\bar{n}=\sum_{i} n_{i} \epsilon_{i} \Delta \epsilon_{i} / \sum_{i} \epsilon_{i} \Delta \epsilon_{i} . \tag{14}
\end{equation*}
$$

The spectral number $\overline{p_{j}}\left(D_{j}\right)$, representing the number of fragments in the diameter interval $D_{j} \pm \Delta D_{j} / 2$, is given by

$$
\begin{equation*}
\overline{p_{j}}=\frac{\sum_{i} n_{j, i} \epsilon_{i} \Delta \epsilon_{i} / \sum_{i} \epsilon_{i} \Delta \epsilon_{i}}{\Delta D_{j}} \tag{15}
\end{equation*}
$$

where $n_{j, i}$ is the number of fragments for excentricity $i$ encountered in the according diameter interval.

The mean number of fragments obtained for all investigated drop pairs is depicted in figure 8 together with values calculated by the Low and List parameterization. The development is very similar for both cases. However, the numerically obtained values are slightly smaller than those from the experiments, mainly for high collision energies. This is, amongst other reasons, due to an insufficient spatial resolution of the computational domain. As shown below in section 4.6, the numerical results are not grid independent with respect to the generation of very small fragment


Figure 8: Mean number of fragments vs. collision energy found from the numerical simulations (stars) and from the experiments of Low and List (1982a)
droplets which appear numerously for high collision energies.

Fragment size distributions in spectral resolution are shown for all investigated drop pairs in appendix A. The comparison to the Low and List parameterization shows both agreement as well as discrepancies. Whereas the agreement between numerical and experimental results is good for emerging larger fragments, large deviations can be observed especially for very small fragments. This finding can be explained by the already mentioned grid dependency. On the other hand, the experimental results may have been influenced by systematic errors which is particularly important if one takes into account the strong dependency on excentricity as it is shown in the following section.

### 4.5 Influence of Excentricity

The number of fragments versus excentricity is plotted exemplarily in figure 9 for 3 pairs with different $C K E$.
As already stated, there is a strong influence of the collision parameter excentricity on the collision outcome. However, this statement is not unambiguous. Looking at high collision energies, a disc mode breakup occurs for low excentricities and multiple small fragments are produced. Increasing excentricity leads to a decreasing number of secondary droplets until the initial drops persist for a grazing collision.
On the other hand, the behaviour in case of medium and low collision energies is contrary. While the two drops coalesce for almost central collisions and persist for grazing collisions, a number of fragment droplets is produced in between.


Figure 9: Fragment number vs. excentricity for pairs of different $C K E$ as indicated

### 4.6 Assessment of Results

Assessing the obtained numerical results, various factors have to be considered. The most relevant ones seem to be both the spatial resolution and the boundary conditions.


Figure 10: Influence of spatial resolution for pair 9, $\epsilon=0.5$ and $\epsilon=0.8 . \Delta x=100 \mu \mathrm{~m}$ (red circles) and $\Delta x=50 \mu \mathrm{~m}$ (blue stars).

In order to elucidate the grid dependency of the results, particular cases have been simulated with doubled spatial resolution, resulting in $\approx 135 \times$ $10^{6}$ control volumes. The results for the standard resolution ( $\Delta x=100 \mu \mathrm{~m}$ ) and the fine resolu-
tion $(\Delta x=50 \mu m)$ are shown in figure 10 for Pair 9, $\epsilon=0.5$ and $\epsilon=0.8$. It is well known that the ability of the Volume of Fluid method which is employed for tracking the interface to correctly reproduce the physical behaviour of small ligaments is quite sensitive to the spatial resolution of the grid. This fact is reflected by the presented results. For both excentricities, there is a higher number of small fragments in case of finer grid resolution. For larger fragments, however, it is important to point out that there is only a minor discrepancy of results applying either a fine or a coarse grid. From a physical point of view it seems feasible to apply a lower radius limit of fragment droplets to be considered as very small droplets may evaporate quickly and thus do not contribute to the coalescence-collision process.
As for the boundary conditions, the drawback of the presented approach with periodic boundary conditions is that the drops are falling in their own wake which is of major importance to large droplets where the aerodynamic influence of the oncoming flow plays an important role for the deformation and the breakup process. Future investigations will therefore be performed with a moving frame of reference, thus facilitating a natural flow approaching the drops.

## 5 CONCLUSION, PERSPECTIVE

The collision process of different pairs of raindrops has been investigated numerically. The drop pairs studied by Low and List (1982a) are amongst the considered pairs. Comparing to their experimental results, there are both agreement as well as discrepancies.
Future investigations will focus on the use of a moving frame of reference with a specific inflow boundary condition. Thus, more realistic simulations are expected. Clearly the according simulations will significantly increase the numerical efforts.
The results presented in this paper are used by Straub et al. (2008) to create a new parameterization of coalescence efficiencies and fragment size distributions.

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## NOMENCLATURE

| CKE | collision energy | J |
| :---: | :---: | :---: |
| $c_{c}$ | no. of coll. leading to coalescence |  |
| c | total number of collisions | - |
| $d$ | (volume equivalent) diameter | m |
| D | fragment diameter | m |
| $E_{c}$ | coalescence efficiency | - |
| $f$ | VOF variable | - |
| $\mathrm{f}_{\gamma}$ | surface tension term | $\mathrm{N} / \mathrm{m}^{3}$ |
| k | body force (gravity) | $\mathrm{m} / \mathrm{s}^{2}$ |
| $m$ | mass | kg |
| $n$ | number of fragments | - |
| $\bar{n}$ | mean number of fragments | - |
| $p$ | pressure | Pa |
| $\overline{p_{j}}$ | spectral number | 1/m |
| $r$ | radius | m |
| $S_{c}$ | surface energy | $J$ |
| $t$ | time | S |
| u | velocity | $\mathrm{m} / \mathrm{s}$ |
| $v$ | vertical velocity | $\mathrm{m} / \mathrm{s}$ |
| W | energy | J |
| x | position | m |
| $\Delta x$ | grid resolution | m |
| Greek |  |  |
| $\delta$ | distance | m |
| $\epsilon$ | excentricity | - |
| $\mu$ | viscosity | kgm/s |
| $\rho$ | density | $\mathrm{kg} / \mathrm{m}^{3}$ |
| $\sigma$ | surface tension | $\mathrm{N} / \mathrm{m}$ |
| Dimensionless quantities |  |  |
| We | Weber number | $\left(=C K E / S_{c}\right)$ |
| Subscripts |  |  |
| 0 | initial |  |
| $g$ | gas |  |
| $i, j$ | indices |  |
| $l$ | liquid |  |
| $L$ | large droplet |  |
| $S$ | small droplet |  |

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## A Spectral numbers



Figure 11: Spectral numbers of fragments as function of fragment diameter for $\mathrm{d}_{L}$ and $\mathrm{d}_{S}$ as indicated. Stars denote present results, lines those according to the parameterization of Low and List (1982b).

